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COMPUTER PROGRAM OF  
DATA REDUCTION PROCEDURES  
FOR FACILITIES USING  $\text{CO}_2$ - $\text{N}_2$ - $\text{O}_2$ -Ar  
EQUILIBRIUM REAL-GAS MIXTURES

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16. Abstract <p>Data reduction procedures for determining free-stream and post-normal-shock flow conditions are presented. These procedures are applicable to flows of CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, or mixtures of these gases and include the effects of dissociation and ionization. The assumption of thermochemical equilibrium free-stream and post-normal-shock flow is made. Although derived primarily to meet the immediate needs of the expansion tube of the Langley hot gas radiation research facility, these procedures are applicable to any supersonic or hypersonic test facility using these gases or mixtures thereof.</p> <p>The data reduction procedures are based on combinations of three of the following flow parameters measured in the immediate vicinity of the test section:</p> <ul style="list-style-type: none"> <li>(1) Stagnation pressure behind normal shock</li> <li>(2) Free-stream static pressure</li> <li>(3) Stagnation-point heat-transfer rate</li> <li>(4) Free-stream velocity</li> <li>(5) Free-stream density</li> </ul> <p>Thus, these procedures do not depend explicitly upon measured or calculated upstream flow parameters. The procedures are incorporated into a single computer program written in FORTRAN IV language. A listing of this computer program is presented, along with a description of the inputs required and a sample of the data printout.</p>					
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COMPUTER PROGRAM OF DATA REDUCTION PROCEDURES FOR  
FACILITIES USING CO<sub>2</sub>-N<sub>2</sub>-O<sub>2</sub>-Ar EQUILIBRIUM  
REAL-GAS MIXTURES

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SUMMARY

Data reduction procedures for determining free-stream and post-normal-shock flow conditions are presented. These procedures are applicable to flows of CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, or mixtures of these gases and include the effects of dissociation and ionization. The assumption of thermochemical equilibrium free-stream and post-normal-shock flow is made. Although derived primarily to meet the immediate needs of the expansion tube of the Langley hot gas radiation research facility, these procedures are applicable to any supersonic or hypersonic test facility using these gases or mixtures thereof.

The data reduction procedures are based on combinations of three of the following flow parameters measured in the immediate vicinity of the test section:

- (1) Stagnation pressure behind normal shock
- (2) Free-stream static pressure
- (3) Stagnation-point heat-transfer rate
- (4) Free-stream velocity
- (5) Free-stream density

Thus, these procedures do not depend explicitly upon measured or calculated upstream flow parameters. The procedures are incorporated into a single computer program written in FORTRAN IV language. A listing of this computer program is presented, along with a description of the inputs required and a sample of the data printout.

INTRODUCTION

As discussed in reference 1, significant differences between measured test-section flow quantities and predicted test-section flow quantities based on upstream flow conditions were observed in the Langley pilot model expansion tube. In order to provide a means for obtaining accurate test-section conditions, a computational scheme based on flow properties measured in the immediate vicinity of the test section was derived in reference 1.

This scheme eliminated an explicit dependence upon measured or calculated upstream flow properties, thereby resulting in a substantial reduction in the uncertainty in predicted test-section flow conditions. The study of reference 1 was, however, limited to thermochemical equilibrium, imperfect, real-air flows.

Experimental investigations made in test facilities for which the test gas will be representative of Mars and Venus atmospheres ( $\text{CO}_2$  predominance) require accurate predictions of test-section flow conditions for such real-gas mixtures. Therefore, the purpose of this program is to provide a means for obtaining accurate test-section conditions for real gases  $\text{CO}_2$ ,  $\text{N}_2$ ,  $\text{O}_2$ , and Ar or mixtures of these gases. This is achieved by employing a computational scheme based on combinations of three flow parameters measured in the immediate vicinity of the test section. The measured flow properties serving as inputs to the data reduction procedures presented herein are as follows:

- (1) Stagnation pressure behind normal shock
- (2) Free-stream static pressure
- (3) Stagnation-point heat-transfer rate
- (4) Free-stream velocity
- (5) Free-stream density

Of the 10 possible data reduction procedures from these inputs, seven are presented herein. (Data reduction procedures deemed less preferable in the error analysis study of ref. 1 are omitted.) The thermodynamic properties for  $\text{CO}_2$ ,  $\text{N}_2$ ,  $\text{O}_2$ , Ar, and mixtures of these gases are obtained from references 2 and 3. Although the data reduction procedures presented herein were derived to meet the immediate needs of the expansion tube of the Langley hot gas radiation research facility, these real-gas-mixture procedures are also applicable to supersonic or hypersonic test facilities using these gases or mixtures of these gases.

The procedures are incorporated into a single computer program written in FORTRAN IV language. A listing of this computer program is presented in appendix A and a description of the inputs required is presented in appendix B. Program output parameters for various gas mixtures are illustrated by sample data printouts presented in appendix C.

## SYMBOLS

The International System of Units (SI) is used for all physical quantities in this study. Conversion factors relating the International System of Units to the U.S. Customary Units are given in reference 4.

$a$	speed of sound, m/sec
$h$	specific enthalpy, $\text{m}^2/\text{sec}^2$ (J/kg)
$M$	Mach number, $U/a$
$N_{Pr}$	Prandtl number
$N_{Re}$	Reynolds number, $\text{m}^{-1}$
$p$	pressure, $\text{N}/\text{m}^2$
$\dot{q}$	heat-transfer rate, $\text{W}/\text{m}^2$
$R$	universal gas constant, $8.31434 \times 10^3 \text{ J}/\text{kmole} \cdot ^\circ\text{K}$
$r$	nose radius, m
$sW_o/R$	nondimensional specific entropy
$T$	temperature, $^\circ\text{K}$
$U$	velocity, m/sec
$W$	molecular weight, kg/kmole
$W_o$	molecular weight of undissociated gas or gas mixture, kg/kmole
$X$	mole fraction, kmole of species $i$ /kmole of mixture
$Y_i$	number of kmole of species $i$ per mass of mixture, kmole of species $i$ /kg of mixture
$Z$	compressibility factor, $pW_o/\rho RT$
$\gamma_E$	isentropic exponent, $\left(\frac{\partial \log p}{\partial \log \rho}\right)_{sW_o/R}$
$\eta$	parameter defined in equation (12), $\text{kg}/\text{m}^{3/2}\text{-sec} \cdot (\text{N}/\text{m}^2)^{1/2}$

$\mu$  viscosity, N-sec/m<sup>2</sup>

$\rho$  density, kg/m<sup>3</sup>

Subscripts:

c calculated

g geometric

i individual species

m measured

mix mixture

prev previous value of a parameter

t stagnation conditions behind normal shock

w model wall

1 free stream

2 static conditions immediately behind normal shock

Approximate value is denoted by  $\sim$ .

## ANALYSIS

Before the discussion of the calculation procedures for determining free-stream and post-normal-shock flow quantities, the source of thermodynamic properties for CO<sub>2</sub>-N<sub>2</sub>-O<sub>2</sub>-Ar gas mixtures in chemical equilibrium employed in this study is discussed. Next, the iterative methods for crossing the standing normal shock are discussed, since these methods are common to all calculation procedures. Finally, the relations used to predict stagnation-point heat-transfer rate are discussed.

## Thermodynamic Properties for Arbitrary Gas Mixtures

Thermodynamic properties for CO<sub>2</sub>-N<sub>2</sub>-O<sub>2</sub>-Ar gas mixtures are obtained from the results of references 2 and 3. These results include dissociation and ionization. Basic assumptions used in obtaining these results are as follows:

- (1) The mixture is composed of ideal gases.
- (2) For diatomic species the rigid-rotor harmonic oscillator model is used with vibrational-rotational corrections for each electronic configuration.
- (3) Only electronic levels with principal quantum number less than or equal to five are included.

The procedure of references 2 and 3 is based upon the free-energy minimization method of reference 5. For a given pressure and temperature, the free energy for individual species are computed from the partition function of statistical mechanics. (The five components and 26 species considered in refs. 2 and 3 are tabulated in appendix B.) The equilibrium composition is then obtained by minimization of the free energy. After the composition for a given pressure and temperature is determined, the corresponding thermodynamic properties of interest are computed directly.

The program of references 2 and 3 is included in the present study as a subroutine and referred to herein as ROGO. The basic inputs to ROGO, other than the atomic energy level constants (which are tabulated in ref. 2), are pressure, temperature, and initial estimates of the species concentrations. For the free-energy minimization method to determine the composition of a gas mixture, the initial estimates of  $Y_i$  are somewhat arbitrary. In the present study, the partial pressures of the CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, and/or Ar test gases in the initial state (prior to addition of energy) are assumed known. The corresponding mole fractions for these gases are obtained from Dalton's law.

$$X_i = \frac{p_i}{p_{\text{mix}}} \quad (1)$$

and the molecular weight is given by

$$W_0 = \sum_i X_i W_i \quad (2)$$

The initial estimates for the species concentrations for CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, and Ar are obtained from

$$Y_i = \frac{X_i}{W_0} \quad (3)$$

For the remaining 22 species, the initial estimates for the concentrations are set equal to  $10^{-20}$ . Thermodynamic properties obtained from ROGO, for a given  $p$  and  $T$ , are  $a$ ,  $h$ ,  $sW_O/R$ ,  $X_i$ ,  $Z$ ,  $\gamma_E$ , and  $\rho$ .

Combinations of input thermodynamic properties other than  $p$  and  $T$  are required in the present study. An iterative-interpolation scheme was derived to enable determination of thermodynamic properties from combinations of  $h$ ,  $p$ ,  $sW_O/R$ , and  $\rho$ . This iterative-interpolation scheme is referred to herein as FIND (I), and the inputs for a given I are as follows:

I	Inputs to FIND (I)
1	$p, \rho$
2	$p, h$
3	$p, sW_O/R$
4	$h, \rho$

In the iterative phase of FIND (1, 2, or 3),  $T$  is varied (for a given  $p$ ) to bring the corresponding  $\rho$ ,  $h$ , or  $sW_O/R$  from ROGO toward agreement with the known  $\rho$ ,  $h$ , or  $sW_O/R$ . This iteration phase is terminated when the uncertainty in  $T$  is reduced to less than  $250^\circ$  K. ROGO is used to obtain the thermodynamic properties at the midpoint and ends of this region of uncertainty. An interpolation is performed over this region to obtain the desired thermodynamic properties. To assist in the reduction of computer time, the flow region (free stream or postshock) is identified in FIND (I). Upper and lower limits on  $T$  for these two regions are inputs. Hence, if the user of this program has a priori approximate values of  $T_1$  and  $T_2$  or  $T_t$ , a reduction in computer time can be realized by establishing these limits on  $T$  (see appendix B); if not, the limits are taken as  $0^\circ$  K to  $8000^\circ$  K for free-stream conditions and  $0^\circ$  K to  $16\,000^\circ$  K for postshock conditions.

For FIND (4), where  $h$  and  $\rho$  are inputs, an initial value of  $p$  is assumed and the iteration-interpolation scheme for FIND (1) employed to determine the thermodynamic properties for this  $p$  (that is, with this  $\tilde{p}$  and  $\rho$ ,  $T$  is varied until the  $\rho$  from ROGO is within 0.1 percent of the input  $\rho$ ). The calculated  $h$  is compared to the input  $h$ ; if not within 0.1 percent,  $p$  is varied and the procedure repeated. This iterative scheme is continued until the condition on  $h$  is satisfied, or the  $\Delta p$  of the iteration becomes less than a given value. If the latter occurs, the iteration is terminated and an interpolation performed to obtain the desired thermodynamic quantities.



### Iterative Procedure for Standing Normal Shock

The conservation relations for mass, momentum, and energy for a standing normal shock are

$$\rho_1 U_1 = \rho_2 U_2 \quad (4)$$

$$p_1 + \rho_1 U_1^2 = p_2 + \rho_2 U_2^2 \quad (5)$$

$$h_1 + \frac{1}{2} U_1^2 = h_2 + \frac{1}{2} U_2^2 \quad (6)$$

Both the direct solution and inverse solution to the conservation relations are used herein.

In the direct solution, the free-stream conditions appearing on the left side of equations (4) to (6) are considered known. The  $h_t$  can be determined from the energy relation (eq. (6))

$$h_t = h_1 + \frac{1}{2} U_1^2 \quad (7)$$

If measured  $p_t$  is not available, the relation (see ref. 1)

$$\tilde{p}_t = 0.97 \rho_1 U_1^2 \quad (8)$$

is used to obtain an accurate estimate of  $p_t$ . From a known  $p_t$  or estimated value from equation (8) and known value of  $h_t$ , a value of  $\rho_t$  is obtained from FIND (2). The initial estimate of  $\rho_2$  is taken to be  $0.955\rho_t$ . This value of  $\rho_2$  is used in equations (4) to (6) to obtain corresponding values of  $p_2$ ,  $h_2$ , and  $U_2$ . The  $p_2$  and  $h_2$  are used as inputs to FIND (2) to obtain a value of  $\rho_2$ . This  $\rho_2$  from FIND (2) is compared to the initial estimate of  $\rho_2$ . If these values are not within 0.1 percent, the  $\rho_2$  obtained from FIND (2) is used in equations (4) to (6) to obtain upgraded values of  $p_2$ ,  $h_2$ , and  $U_2$ . This method of successive approximations is repeated until successive values of  $\rho_2$  from FIND (2) are within 0.1 percent.

The postshock stagnation conditions are determined by assuming that the flow region immediately behind the normal shock to the stagnation point is isentropic (that is,  $\frac{s_t W_0}{R} = \frac{s_2 W_0}{R}$ ). Now, the variation in conditions from immediately downstream of the

shock to the stagnation point is relatively small (that is,  $\gamma_{E,2} \approx \gamma_{E,t}$  and  $Z_2 \approx Z_t$ ). Thus, this region may be considered to behave as a calorically perfect gas. The  $p_t$  can be accurately estimated from the ideal-gas isentropic relation

$$\tilde{p}_t = p_2 \left( 1 + \frac{\gamma_{E,2} - 1}{2} M_2^2 \right)^{\gamma_{E,2}/\gamma_{E,2} - 1} \quad (9)$$

This  $\tilde{p}_t$  is used as an input to FIND (2), in conjunction with  $h_t$ , to obtain a value of  $s_t W_o/R$ . If this  $s_t W_o/R$  is not within 0.05 percent of  $s_2 W_o/R$ , the  $p_t$  is varied (upward or downward) 4 percent in 1-percent increments. The values of  $s_t W_o/R$  corresponding to each  $p_t$  and the  $h_t$  are obtained from FIND (2). The value of  $p_t$  resulting in  $\frac{s_t W_o}{R} = \frac{s_2 W_o}{R}$  is obtained by interpolation.

In the inverse solution, the stagnation-point conditions are obtained from FIND (2) where inferred  $h_t$  from stagnation-point heat-transfer rate measurement and measured  $p_t$  serve as inputs. An estimate of  $p_2$  is made and used with  $s_t W_o/R$  as inputs to FIND (3) to obtain  $\rho_2$  and  $h_2$ . The corresponding  $U_2$  is obtained from the energy relation (eq. (6))

$$U_2 = \sqrt{2(h_t - h_2)} \quad (10)$$

In the procedures using the inverse solution, either  $p_1$  or  $\rho_1$  is known. Thus, the free-stream quantities on the left side of equations (4) to (6) can be determined. The  $p_1$  and  $\rho_1$  are used in FIND (1) to obtain a value of  $h_1$ . This  $h_1$  from FIND (1) is compared to the calculated  $h_1$  from equation (6) and, if not within 0.1 percent, the  $p_2$  is varied and the procedure repeated. This numerical iteration on  $p_2$  is continued until the convergence criterion on  $h_1$  is satisfied.

### Prediction of Stagnation-Point Heat-Transfer Rates

Because measured  $\dot{q}_t$  is a basic input datum, it is necessary that a relatively accurate means for predicting  $\dot{q}_t$  in  $\text{CO}_2\text{-N}_2\text{-O}_2\text{-Ar}$  mixtures be available. Considerable effort has been directed toward obtainment of expressions for predicting  $\dot{q}_t$  at high velocities in air. In comparison, the number of similar studies in arbitrary gas mixtures is relatively small.

Recently, however, an analytical study of stagnation-point convective heat transfer to an axisymmetric blunt body was performed for a number of gas mixtures in thermo-

chemical equilibrium (ref. 6). This study demonstrated that the simple, empirical relation of reference 7 for predicting  $\dot{q}_t$  in Ar-H<sub>2</sub>-N<sub>2</sub>-CO<sub>2</sub> gas mixtures yields results which are in good agreement with analytical results, provided the  $N_{Pr,w}$  of the individual gases are approximately equal. For the gases considered herein,  $N_{Pr,w}$  varies from approximately 0.67 for Ar to approximately 0.7 for N<sub>2</sub> and O<sub>2</sub> and to approximately 0.72 for CO<sub>2</sub> at the  $T_w$  of interest ( $T_w$  from room temperature to 1500° K). Hence, according to reference 6, the empirical relation of reference 7 should provide relatively accurate predictions of  $\dot{q}_t$  for the present gas mixtures. This relation of reference 7, which was also employed in the air study of reference 1, is

$$\dot{q}_t = \eta \sqrt{\frac{p_t}{r_g}} (h_t - h_w) \quad (11)$$

where

$$\eta = W_o \left( \sum_i \frac{X_i W_i}{\eta_i} \right)^{-1} \quad (12)$$

and the  $\eta_i$  are given in the following table:

Species i	$\eta_i$
CO <sub>2</sub>	$4.3102 \times 10^{-4}$
N <sub>2</sub>	3.6285
O <sub>2</sub>	4.8945
Ar	5.4788

(The value of  $\eta_i$  for O<sub>2</sub> is not presented in ref. 7. This value was deduced by comparison of the  $K_i$  of table I in ref. 7 for air to the  $K_i$  for an air mixture of CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, and Ar. The air-mixture composition was taken as 78.084 percent N<sub>2</sub>, 20.946 percent O<sub>2</sub>, 0.937 percent Ar, and 0.033 percent CO<sub>2</sub> by volume (ref. 1).) The  $h_w$  is obtained directly from ROGO, where the required temperature input to ROGO is  $T_w$ . For the range of  $T_w$  considered herein (300° K <  $T_w$  < 1500° K),  $h_w$  may be considered to be a function of  $T_w$  only and a precise knowledge of  $p_w$  is not necessary for obtaining  $h_w$  accurately. For procedures where  $(p_t)_m$  is an input or  $\tilde{p}_t$  can be obtained from equation (8), the  $p_w$  is equal to  $(p_t)_m$  or  $(p_t)_c$ . (For the single procedure where  $(p_t)_m$  is not an input, as well as  $(\rho_1)_m$  and  $(U_1)_m$  (that is,  $\tilde{p}_t$  cannot be obtained from eq. (8)),  $p_w$  is simply set equal to  $1.01325 \times 10^5$  N/m<sup>2</sup>.)

## Procedures for Determining Free-Stream and Postshock Conditions

The procedures for determining free-stream and post-normal-shock flow conditions are identified in the computer program by ITEST. For convenience, this method of identification is employed in the following discussion. The basic measured inputs and iterative procedure for crossing the normal shock are given in the following table:

ITEST	Measured inputs	Shock-crossing procedure
1	$p_1, U_1, p_t$	Direct
2	$p_1, p_t, \dot{q}_t$	Inverse
3	$p_1, \rho_1, U_1$	Direct
4	$p_1, \rho_1, p_t$	Direct
5	$\rho_1, p_t, \dot{q}_t$	Inverse
6	$p_1, \rho_1, \dot{q}_t$	Direct
7	$\rho_1, U_1, \dot{q}_t$	Direct

Of the 10 possible combinations of the input parameters  $p_1, \rho_1, U_1, p_t$ , and  $\dot{q}_t$ , three have been omitted from the present study. The procedure involving inputs  $\rho_1, U_1$ , and  $p_t$  was omitted because of the existence of a relatively accurate expression (eq. (8)) relating all three quantities. Omission of the other two procedures ( $U_1, p_t, \dot{q}_t$ , and  $p_1, U_1, \dot{q}_t$ ) was based on the error analysis performed in reference 1, which showed these procedures to be less acceptable than others.

The individual procedures are now discussed briefly.

ITEST = 1.— A value of  $\tilde{\rho}_1$  is determined from the measured  $U_1$  and  $p_t$  by using equation (8). The measured  $p_1$  and this  $\tilde{\rho}_1$  are used as inputs to FIND (1) to obtain the corresponding free-stream thermodynamic properties. The direct iterative shock-crossing procedure is performed. The calculated  $p_t$  is compared to the measured  $p_t$  and if not within a prescribed tolerance (TOLPT),  $\tilde{\rho}_1$  is adjusted by using the relation

$$\tilde{\rho}_1 = (\tilde{\rho}_1)_{\text{prev}} \frac{(p_t)_m}{(p_t)_{c,\text{prev}}} \quad (13)$$

This new value of  $\tilde{\rho}_1$  is used, in conjunction with  $(p_1)_m$ , as input into FIND (1). The corresponding value of  $h_1$  obtained from FIND (1) is used in the direct shock-crossing solution. The  $(p_t)_c$  is again compared to  $(p_t)_m$ . This procedure of upgrading

$\tilde{p}_1$  according to equation (13) is continued until  $(p_t)_c$  is within TOLPT of  $(p_t)_m$ . (Note that  $\tilde{p}_1$  from eq. (8) was used only to obtain a relatively accurate first estimate of  $h_1$  and is not involved in the final phase of upgrading  $\rho_1$ .)

ITEST = 2.- Since  $p_t$  and  $\dot{q}_t$  are measured quantities and  $r_g$  and  $T_w$  are considered known, the  $h_t$  is determined from equation (11). This  $h_t$  and the measured  $p_t$  are used as inputs to FIND (2) to obtain the postshock stagnation conditions. The inverse iterative shock-crossing procedure is performed, where  $(p_1)_m$  is the known free-stream flow quantity, to obtain the corresponding static conditions immediately behind the normal shock and the free-stream conditions.

ITEST = 3.- The measured  $p_1$  and  $\rho_1$  are used as inputs to FIND (1) to obtain the corresponding free-stream conditions. After the free-stream thermodynamic properties are determined and  $U_1$  known, the postshock conditions are obtained from the direct shock-crossing procedure.

ITEST = 4.- The  $\tilde{U}_1$  is determined from equation (8) and the free-stream thermodynamic properties are obtained from FIND (1) with the measured  $p_1$  and  $\rho_1$  as inputs. The  $(p_t)_c$  is obtained from the direct shock-crossing procedure and compared to  $(p_t)_m$ . If not within the desired tolerance (TOLPT), the  $\tilde{U}_1$  is upgraded according to

$$\tilde{U}_1 = (\tilde{U}_1)_{\text{prev}} \sqrt{\frac{(p_t)_m}{(p_t)_{c,\text{prev}}}} \quad (14)$$

This new value of  $\tilde{U}_1$  is used in the direct shock-crossing solution. The  $U_1$  is upgraded according to equation (14) until  $(p_t)_c$  is within TOLPT of  $(p_t)_m$ .

ITEST = 5.- The procedure of ITEST = 5 is similar to that of ITEST = 2, the only difference being that  $\rho_1$  (instead of  $p_1$ ) is used as the required known free-stream flow quantity in the inverse shock-crossing solution.

ITEST = 6.- The free-stream thermodynamic quantities are obtained from FIND (1) with inputs  $(p_1)_m$  and  $(\rho_1)_m$ . A  $\tilde{U}_1$  is obtained by combining equations (7), (8), and (11) to give

$$\tilde{U}_1^3 + 2(h_1 - h_w)\tilde{U}_1 = \frac{2(\dot{q}_t)_m}{\eta} \sqrt{\frac{r_g}{0.97(\rho_1)_m}} \quad (15)$$

The  $\tilde{U}_1$  from equation (15) is relatively accurate, the only uncertainty being in the value of 0.97 appearing in the last term. With a value of  $\tilde{U}_1$ , the postshock conditions are

determined as discussed in ITEST = 3. The value of 0.97 appearing in equation (15) is compared with

$$C_1 = \frac{p_t}{\rho_1 U_1^2} \quad (16)$$

If not within 0.1 percent, the value 0.97 in equation (15) is replaced by  $C_1$  of equation (16) and the calculation procedure repeated.

ITEST = 7. - In order to estimate a value of  $h_1$ , equation (15) is rearranged to give

$$\tilde{h}_1 = h_w + \frac{(\dot{q}_t)_m}{\eta} \sqrt{\frac{r_g}{0.97(\rho_1)_m (U_1)_m^2} - \frac{1}{2}(U_1)_m^2} \quad (17)$$

Again, the value of 0.97 appearing under the square root is the only uncertainty in this expression. The free-stream thermodynamic quantities are obtained from FIND (4) with  $(\rho_1)_m$  and  $\tilde{h}_1$  as inputs. The postshock conditions are determined as discussed in ITEST = 3. The value of 0.97 appearing in equation (17) is compared with  $C_1$  of equation (16). If not within 0.1 percent, the value 0.97 in equation (17) is replaced by  $C_1$  of equation (16) and the procedure repeated.

In many flow studies, the parameters free-stream Mach number and free-stream unit Reynolds number are of interest. These two parameters are determined in each procedure. The  $M_1$  is obtained simply by dividing  $U_1$  by  $a_1$ . The  $N_{Re,1}$  is defined as  $\rho_1 U_1 / \mu_1$ ; hence  $\mu_1$  must be determined. The viscosity of a gas mixture of n-components may be approximated by the relation (see ref. 8)

$$\mu = \sum_{i=1}^n \frac{\mu_i}{1 + \sum_{\substack{j=1 \\ j \neq i}}^n \Phi_{ij} \frac{X_j}{X_i}} \quad (18)$$

where

$$\Phi_{ij} = \frac{\left[ 1 + \left( \frac{\mu_i}{\mu_j} \right)^{1/2} \left( \frac{W_j}{W_i} \right)^{1/4} \right]^2}{2\sqrt{2} \left( 1 + \frac{W_i}{W_j} \right)^{1/2}} \quad (19)$$

In the present study, the number of components is taken to be four. These components correspond to the initial composition of Ar, CO<sub>2</sub>, N<sub>2</sub>, and O<sub>2</sub> (that is, the  $W_i$  and  $W_j$  of eq. (19) correspond to the  $W_0$  of the four gases under consideration).

The viscosity for Ar was obtained by applying a curve fit to the results of reference 9, which includes data from a number of sources. The resulting expression is

$$\mu = 3.33 \times 10^{-7} T^{0.739} \quad (20)$$

This expression yields values of  $\mu$  within 10 percent of the results illustrated in reference 9, for the temperature range of 150° K to 5000° K.

Simple expressions for the viscosity, in the form

$$\mu = (a_0 + a_1 T + a_2 T^2) \times 10^{-7} \quad (21)$$

were obtained for CO<sub>2</sub>, N<sub>2</sub>, and O<sub>2</sub> for temperature ranges of 150° K to 1000° K and 1000° K to 5000° K. The constants ( $a_0$ ,  $a_1$ , and  $a_2$ ) of equation (21) are presented in the following table, along with the source used in obtaining these constants:

Gas	$\Delta T$	$a_0$	$a_1$	$a_2$	Ref.
CO <sub>2</sub>	150 to 1000	$-9.7303 \times 10^{-1}$	$5.5222 \times 10^{-1}$	$-1.6139 \times 10^{-4}$	10
CO <sub>2</sub>	1000 to 5000	$1.5029 \times 10^2$	$2.4890 \times 10^{-1}$	$-6.1747 \times 10^{-6}$	10, 11
N <sub>2</sub>	150 to 1000	$2.2992 \times 10^1$	$5.5586 \times 10^{-1}$	$-1.8436 \times 10^{-4}$	10, 12
N <sub>2</sub>	1000 to 5000	$1.6388 \times 10^2$	$2.4601 \times 10^{-1}$	$-7.7388 \times 10^{-6}$	10, 13
O <sub>2</sub>	150 to 1000	$1.9939 \times 10^1$	$6.6236 \times 10^{-1}$	$-2.0410 \times 10^{-4}$	10
O <sub>2</sub>	1000 to 5000	$2.3030 \times 10^2$	$2.5597 \times 10^{-1}$	$-2.2643 \times 10^{-6}$	10, 14

Viscosities for temperatures from 150° K to 5000° K were calculated for air ( $X_{Ar} = 9.37 \times 10^{-3}$ ,  $X_{CO_2} = 3.3 \times 10^{-4}$ ,  $X_{N_2} = 7.8084 \times 10^{-1}$ , and  $X_{O_2} = 2.0946 \times 10^{-1}$ ) by using equation (18) and compared to values from reference 1. This comparison showed that the values of  $\mu$  from equation (18) were within 3 percent of those of reference 1 for this temperature range. For mixtures where Ar or N<sub>2</sub> predominate, equation (18) should provide reasonably accurate values of  $\mu$  for temperatures up to 5000° K. For mixtures where CO<sub>2</sub> or O<sub>2</sub> predominate, the  $\mu$  of equation (18) will contain somewhat larger uncertainties at  $T \gtrsim 2000^\circ$  K because of dissociation of the CO<sub>2</sub> or O<sub>2</sub>. For example, reference 11 shows that for  $T \gtrsim 1700^\circ$  K, the  $\mu_{CO_2}$  has a pressure dependence because of dissociation of CO<sub>2</sub>. However, variation in pressure from  $10^2$  to  $10^6$  N/m<sup>2</sup>, for a given

temperature, results in a maximum uncertainty in  $\mu_{\text{CO}_2}$  of less than 10 percent for temperatures less than  $5000^\circ \text{K}$  (ref. 11). Thus, equation (18) should provide values of  $\mu$ , for mixtures where  $\text{CO}_2$  or  $\text{O}_2$  predominate, of sufficient accuracy for many flow studies. (Eq. (18) was employed for the Mars model of ref. 11 ( $X_{\text{Ar}} = 0.32$ ,  $X_{\text{CO}_2} = 0.43$ , and  $X_{\text{N}_2} = 0.25$ ) and a temperature range of  $1000^\circ \text{K}$  to  $5000^\circ \text{K}$ . These  $\mu$  from eq. (18) were within 6 percent of those presented in ref. 11 for  $p = 10^5 \text{ N/m}^2$  for this temperature range.)

## DISCUSSION

Because of the greater simplicity associated with procedure  $\text{ITEST} = 3$ , this procedure was the first to be examined. A check case was run with air (78.084 percent  $\text{N}_2$ , 20.946 percent  $\text{O}_2$ , 0.937 percent Ar, and 0.033 percent  $\text{CO}_2$  by volume) as the test gas. The inputs  $p_1$ ,  $\rho_1$ , and  $U_1$  were the same values as used in obtaining the sample printout of reference 1. Comparison of these results for  $\text{ITEST} = 3$  to the sample printout case of reference 1 showed excellent agreement. The 15.24-km/sec entry trajectory cases presented in reference 1 were run with the present  $\text{ITEST} = 3$  procedure and the preceding air model. For this trajectory, which encompassed a range of  $T_t$  from  $1500^\circ \text{K}$  to  $12\,000^\circ \text{K}$ , excellent agreement was observed between the present results and those of reference 1. Following the successful check of  $\text{ITEST} = 3$ , the remaining six procedures were run with a common check case. These check cases used the same free-stream inputs as  $\text{ITEST} = 3$ , but used the calculated postshock outputs  $p_t$  and  $\dot{q}_t$  of  $\text{ITEST} = 3$  as inputs. For these check cases,  $\text{TOLPT} = 0.001$  and  $\text{TOLQT} = 0.005$ . The computed flow quantities for all six procedures were observed to be in agreement with those of  $\text{ITEST} = 3$ .

Additional cases were run with  $\text{ITEST} = 3$  for mixtures of 95 percent  $\text{CO}_2$  and 5 percent  $\text{N}_2$  (representative of Venus) and 85 percent  $\text{CO}_2$ , 1 percent  $\text{N}_2$ , and 14 percent Ar (representative of Mars). The free-stream inputs were the same as those employed in the check case for  $\text{ITEST} = 3$  and are representative of an expansion tube test in air with heated helium driver. The results of these additional cases are presented in the sample printouts of appendix C.

In order to examine the relative total computer time (computational and peripheral) required by the various procedures, each procedure was run on a Control Data 6600 computer system. The representative expansion-tube test case for air used in the computer time study of reference 1 was also used in the present time study. The limits on temperature for FIND (I) (see appendix B) were as follows:

$$\text{TMAX1} = 1500^\circ \text{K}$$

$$\text{TMAX2} = 8000^\circ \text{K}$$



$$TMIN1 = 200^{\circ} \text{ K}$$

$$TMIN2 = 5000^{\circ} \text{ K}$$

The total computer times for each procedure were obtained for the case where all 26 species (see appendix B) were considered and for the case where the air model was simplified to 10 species ( $e^{-}$ , Ar, N,  $N^{+}$ ,  $N_2$ , O,  $O^{+}$ ,  $O_2$ , NO,  $NO^{+}$ ). The times for these two cases are given in the following table:

ITEST	Total computer time, sec	
	26-species model	10-species model
1	125	70
2	250	120
3	80	45
4	110	65
5	300	125
6	80	45
7	125	70

The reduction in computer time for the simplified air model is illustrated by this table. For the test case used in this time study, elimination of the 16 species between the two air models did not introduce significant variations (greater than 0.5 percent) in calculated free-stream and postshock conditions. (See printout of appendix C for 26-species air model and 10-species air model.) This result is not surprising since the percent by volume of  $CO_2$  in the initial air composition for the 26-species model was relatively small (0.033 percent); hence elimination of  $CO_2$  from the initial composition should not significantly influence the calculated flow quantities. (Elimination of  $CO_2$  from the initial air composition corresponds to a reduction of eight species, since the C-element is eliminated.) Examination of the mole fractions at the stagnation-point conditions for the 26-species air model shows that the dependence on doubly ionized species along with  $O^{-}$ ,  $Ar^{+}$ ,  $N_2^{+}$ ,  $O_2^{+}$ , and  $O_2^{-}$  is much less than the remaining species; thus, elimination of these species should also not significantly influence the calculated flow quantities for the test case being considered. Therefore, judicious selection of species can result in a substantial reduction in computer time without appreciable loss in accuracy. (See appendix B for discussion of variation in the number of species as required in the present computer program.)

## CONCLUDING REMARKS

Data reduction procedures for determining free-stream and post-normal-shock flow conditions are presented. These procedures are applicable to flows of CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, or mixtures of these gases and include the effects of dissociation and ionization. The assumption of thermochemical equilibrium flow is made. Although derived primarily to meet the immediate needs of the expansion tube of the Langley hot gas radiation research facility, these procedures are applicable to any supersonic or hypersonic test facility using these gases or mixtures thereof.

These procedures are based on the following flow parameters measured in the immediate vicinity of the test section:

- (1) Stagnation pressure behind normal shock
- (2) Free-stream static pressure
- (3) Stagnation-point heat-transfer rate
- (4) Free-stream velocity
- (5) Free-stream density

The various combinations of measured flow parameters are identified herein as ITEST and are:

<u>ITEST</u>	<u>Measured flow parameter</u>
1	(1), (2), (4)
2	(1), (2), (3)
3	(2), (4), (5)
4	(1), (2), (5)
5	(1), (3), (5)
6	(2), (3), (5)
7	(3), (4), (5)

These seven procedures are incorporated into a single computer program written in FORTRAN IV language.

Cases run with procedure ITEST = 3 for an air mixture were observed to be in good agreement with the results of the real-air study of NASA TN D-6618 for stagnation temperatures from 1500° K to 12 000° K.

A computer time study for each procedure showed that a substantial reduction in computer time, without appreciable loss in accuracy, may be realized in many cases by judicious selection of the number of species.

Langley Research Center,  
National Aeronautics and Space Administration,  
Hampton, Va., February 2, 1972.

## APPENDIX A

### LISTING OF COMPUTER PROGRAM

The data reduction procedures for determining free-stream and post-normal-shock flow conditions for CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, or mixtures of these gases are incorporated into a single computer program. This program is written in FORTRAN IV language for the Control Data 6600 computer system. Machine requirements are 70 000-octal locations of core storage. A listing of the main program (MILLER) and subroutines FIND (I) and ROGO, with comments, is reproduced in the following pages.

# APPENDIX A - Continued

JOB,1,1000,070000,500.	A3238	RGK143	1247A	CENT
USER,MILLER, CHARLES G III	000605575N	34540		
RUN(S).				
SETINDF.				
LGO.				
-				
PROGRAM MILLER(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)				A 1
C DATA REDUCTION PROCEDURE FOR C02-N2-O2-AR MIXTURES				A 2
C THERMODYNAMIC PROPERTIES OBTAINED FROM PROGRAM OF ALLISON				A 3
C THERMOCHEMICAL EQUILIBRIUM ASSUMED				A 4
C				A 5
COMMON NUMSP,JINDX,IAR,IN2,IO2,IC02,BOZ,XAR,XN2,X02,XC02				A 6
COMMON TMAX1,TMAX2,TMIN1,TMIN2				A 7
COMMON XMOLE(30),SPECIE(30)				A 8
DIMENSION TABP(5), TABR(5), TABSR(5), TABT(5), TABA(5), TABZ(5), T				A 9
1ABG(5)				A 10
DIMENSION COEFS(4), ROOTS(6), TEMP(14)				A 11
DIMENSION VIS(4), W(4), XMF(4), PHI(4,4), SUM(4,4), SUMM(4)				A 12
DIMENSION RESULT(2)				A 13
REAL M1,M2,MU				A 14
NAMelist /INP/ PTM,PJM,UIM,QTM,RHO1M,RN,ITEST,TWE,PC02,PN2,PO2,PAR				A 15
1,PMIX,RUN,TOLPT,TMAX1,TMAX2,TMIN1,TMIN2,TOLQT,NUMSP,JINDX,IAR,IN2,				A 16
2IO2,IC02				A 17
BOZ=0.				A 18
CALL DAYTIM (RESULT)				A 19
1 PC02=PN2=PO2=PAR=PTM=PIM=UIM=QTM=RHO1M=QTHOS=0.0				A 20
TMAX1=TMAX2=TMIN1=TMIN2=0.0				
IAR=IN2=IO2=IC02=0				
TOLPT=.001				
TOLQT=.005				
TWE=.00.				
RN=.01				
READ (5,INP)				A 21
IF (FNDFILE 5) 49,2				A 22
2 PRINT 50, RESULT(1)				A 23
PRINT 51				A 24
PRINT 52				A 25
PRINT 53				A 26
XC02=PC02/PMIX				A 27
XN2=PN2/PMIX				A 28
X02=PO2/PMIX				A 29
XAR=PAR/PMIX				A 30
MU=44.011*XC02+28.016*XN2+32.*X02+39.944*XAR				A 31
PRINT 54				A 32

# APPENDIX A - Continued

	PRINT 55. RUN,P1M,U1M,PTM,OTM,RHO1M,MU,XCO2,XN2,XO2,XAR	A 33
	P1=P1M	A 34
	U1=U1M	A 35
	PT=PTM	A 36
	QT=OTM	A 37
	RHO1=RHO1M	A 38
	ZMIX=1.E+4*(7.2906*XAR+10.2109*XCO2+7.7211*XN2+6.53795*XO2)/MU	A 39
	TW=TWE	A 40
	GO TO (4,4,5,4,4,3,5), ITEST	A 41
3	PWR=1.	A 42
	GO TO 6	A 43
4	PWR=PTM/1.01325E+5	A 44
	GO TO 6	A 45
5	PWR=(.97*RHO1M*U1M**2)/1.01325E+5	A 46
6	CALL ROGO (PWR,RHOW,HWSR,TW,AW,ZW,GAMEW,MU)	A 47
C		A 48
C	INPUTS FOR ITEST=1 ARE P1M,U1M, AND PTM	A 49
C	INPUTS FOR ITEST=2 ARE P1M,PTM, AND QTM	A 50
C	INPUTS FOR ITEST=3 ARE P1M,U1M, AND RHO1M	A 51
C	INPUTS FOR ITEST=4 ARE P1M,PTM, AND RHO1M	A 52
C	INPUTS FOR ITEST=5 ARE PTM,QTM, AND RHO1M	A 53
C	INPUTS FOR ITEST=6 ARE P1M,RHO1M, AND QTM	A 54
C	INPUTS FOR ITEST=7 ARE QTM,RHO1M, AND U1M	A 55
C		A 56
	GO TO (7,8,15,24,8,15,22), ITEST	A 57
C		A 58
C	ESTIMATING PRE-SHOCK CONDITIONS FOR ITEST=1	A 59
C		A 60
7	RHOEST=PTM/(.97*U1M**2)	A 61
	CALL FIND (P1M,RHOEST,H1,S1R,T1,A1,Z1,GAME1,MU,1,1,1)	A 62
	RHO1=RHOEST	A 63
	GO TO 25	A 64
C		A 65
C	ESTIMATING POST-SHOCK STAGNATION CONDITIONS FOR ITEST=2 AND 5	A 66
C		A 67
C	ESTIMATING HT USING ZOBY RELATION(NASA TN D-4799)	A 68
C		A 69
8	HT=ZMIX*QT*SQRT(RN/PT)+HW	A 70
	CALL FIND (PT,RHOT,HT,STR,TT,AT,ZT,GAME1,MU,2,2,2)	A 71
	GO TO 44	A 72
C		A 73
C	PERFORMING STANDING NORMAL SHOCK CROSSING, POST-TO-PRE	A 74
C		A 75
9	MM=0	A 76

# APPENDIX A - Continued

	MN=0	A 77
	S2R=STR	A 78
	PLOW=.84*PT	A 79
	PUP=.98*PT	A 80
	P2=(PUP-PLOW)/2.+PLOW	A 81
	DELP=(PUP-PLOW)/2.	A 82
10	IF (MM.EQ.0.AND.MM.EQ.0) GO TO 11	A 83
	P2=PUP-DELP	A 84
11	CALL FIND (P2,RHO2,H2,STR,T2,A2,Z2,GAME2,MU,3,2)	A 85
	U2=SQRT(2.*(HT-H2))	A 86
	M2=U2/A2	A 87
	BINV=RHO2*U2	A 88
	CINV=P2+BINV*U2	A 89
	IF (ITEST.EQ.2) GO TO 14	A 90
C		A 91
C	CASE WHEN RHO1 IS AN INPUT	A 92
C		A 93
	U1=BINV/RHO1	A 94
	P1=CINV-BINV*U1	A 95
	IF (P1.LT.1.) GO TO 13	A 96
	H1=HT-.5*U1**2	A 97
12	CALL FIND (P1,RHO1,H1E,SIR,T1,A1,Z1,GAME1,MU,1,1)	A 98
	IF (MM.EQ.20) GO TO 46	A 99
	MM=MM+1	A 100
C		A 101
C	CONVERGENCE TEST ON H1	A 102
C		A 103
	IF (ABS(1.-H1/H1E).LE..0015) GO TO 33	A 104
	IF (H1.GT.H1E) GO TO 13	A 105
	PUP=P2	A 106
	PLOW=P2-DELP	A 107
	MN=MN+1	A 108
	GO TO 10	A 109
13	PLOW=P2	A 110
	PUP=P2+DELP	A 111
	MN=MN+1	A 112
	GO TO 10	A 113
C		A 114
C	CASE WHEN P1 IS AN INPUT	A 115
C		A 116
14	U1=(CINV-P1)/BINV	A 117
	RHO1=BINV/U1	A 118
	H1=HT-.5*U1**2	A 119
	GO TO 12	A 120

# APPENDIX A - Continued

C		A 121
C	DETERMINING PRE-SHOCK CONDITIONS FOR ITEST=3 AND 6	A 122
C		A 123
15	CALL FIND (P1M,RHO1M,H1,S1R,T1,A1,Z1,GAME1,MU,1,1)	A 124
	IF (ITEST.EQ.3) GO TO 25	A 125
	CON6=.97	A 126
	NNN=0	A 127
	COEFS(1)=1.	A 128
	COEFS(2)=0.	A 129
	COEFS(3)=2.*(H1-HW)	A 130
16	COEFS(4)=-2.*QTM*ZMIX*SQRT(RN/(CON6*RHO1M))	A 131
	CALL FALG (COEFS,3,0,ROOTS,TEMP,IERR)	A 132
	IF (IERR.NE.0) GO TO 21	A 133
	NNN=NNN+1	A 134
	IF (ABS(ROOTS(2)).LT.1.E-20) GO TO 17	A 135
	IF (ABS(ROOTS(4)).LT.1.E-20) GO TO 19	A 136
	IF (ABS(ROOTS(6)).LT.1.E-20) GO TO 20	A 137
	PRINT 56	A 138
	GO TO 1	A 139
17	U1=ROOTS(1)	A 140
	IF (ABS(ROOTS(4)).GT.1.E-20.AND.ABS(ROOTS(6)).GT.1.E-20) GO TO 25	A 141
18	PRINT 57	A 142
	GO TO 1	A 143
19	U1=ROOTS(3)	A 144
	IF (ABS(ROOTS(6)).GT.1.E-20) GO TO 25	A 145
	GO TO 18	A 146
20	U1=ROOTS(5)	A 147
	GO TO 25	A 148
21	PRINT 58	A 149
	GO TO 1	A 150
C		A 151
C	ESTIMATING PRE-SHOCK CONDITIONS FOR ITEST=7	A 152
C		A 153
22	CON7=.97	A 154
	MMM=0	A 155
23	H1EST=ZMIX*QTM*SQRT(RN/(CON7*RHO1M*U1M**2))+HW-.5*U1M**2	A 156
	H1=H1EST	A 157
	CALL FIND (P1,RHO1M,H1,S1R,T1,A1,Z1,GAME1,MU,4,1)	A 158
	MMM=MMM+1	A 159
	GO TO 25	A 160
C		A 161
C	DETERMINING PRE-SHOCK CONDITIONS FOR ITEST=4	A 162
C		A 163
24	CALL FIND (P1M,RHO1M,H1,S1R,T1,A1,Z1,GAME1,MU,1,1)	A 164



# APPENDIX A - Continued

	U1=SQRT(P1/(.97*RHO1))	A 165
C		A 166
C	PERFORMING STANDING NORMAL SHOCK CROSSING, PRE-TO-POST	A 167
C		A 168
25	BSNS=RHO1*U1	A 169
	CSNS=P1+BSNS*U1	A 170
	DSNS=H1+.5*U1**2	A 171
	HT=DSNS	A 172
	PTEST=.965*RHO1*U1**2	A 173
	CALL FIND (PTEST,RHOT,HT,STR,TT,AT,ZT,GAMET,MU,2,2)	A 174
	RHO2=.955*RHOT	A 175
26	U2=BSNS/RHO2	A 176
	P2=CSNS-BSNS*U2	A 177
	H2=DSNS-.5*U2**2	A 178
	CALL FIND (P2,RNEW,H2,S2R,T2,A2,Z2,GAME2,MU,2,2)	A 179
	IF (ABS(1.-RHO2/RNEW).LE..001) GO TO 27	A 180
	RHO2=RNEW	A 181
	GO TO 26	A 182
27	RHO2=RNEW	A 183
	M2=U2/A2	A 184
	PTCAL=P2*(1.+((GAME2-1.)/2.)*M2**2)**(GAME2/(GAME2-1.))	A 185
	CALL FIND (PTCAL,RHOT,HT,STR,TT,AT,ZT,GAMET,MU,2,2)	A 186
	IF (ABS(1.-S2R/STR).LE..0005) GO TO 31	A 187
	TABP(1)=PTCAL	A 188
	TABR(1)=RHOT	A 189
	TABSR(1)=STR	A 190
	TART(1)=TT	A 191
	TABA(1)=AT	A 192
	TABZ(1)=ZT	A 193
	TABG(1)=GAMET	A 194
	IF (STR.LT.S2R) GO TO 28	A 195
	CON=.01	A 196
	N=-2	A 197
	GO TO 29	A 198
28	CON=-.01	A 199
	N=2	A 200
29	YX=1.+CON	A 201
	DO 30 I=2,5	A 202
	TABP(1)=XX*PTCAL	A 203
	PTIN=TABP(1)	A 204
	CALL FIND (PTIN,RHOT,HT,STR,TT,AT,ZT,GAMET,MU,2,2)	A 205
	TABR(1)=RHOT	A 206
	TABSR(1)=STR	A 207
	TABT(1)=TT	A 208

# APPENDIX A - Continued

	TABA(I)=AT	A 209
	TABZ(I)=ZT	A 210
	TABG(I)=GAMET	A 211
	XX=XX+CON	A 212
30	CONTINUE	A 213
	CALL FTLUP (S2R,PTCAL,N.5,TABSR,TABP)	A 214
	CALL FTLUP (S2R,RHOT,N.5,TABSR,TABR)	A 215
	CALL FTLUP (S2R,TT,N.5,TABSR,TABT)	A 216
	CALL FTLUP (S2R,AT,N.5,TABSR,TABA)	A 217
	CALL FTLUP (S2R,ZT,N.5,TABSR,TABZ)	A 218
	CALL FTLUP (S2R,GAMET,N.5,TABSR,TABG)	A 219
	STR=52R	A 220
C		A 221
31	PT=PTCAL	A 222
	IF (ITEST.EQ.3.OR.ITEST.EQ.6) GO TO 33	A 223
	IF (ITEST.EQ.7) GO TO 33	A 224
	IF (ABS(1.-PTM/PT).LE.TOLPT) GO TO 33	A 225
	IF (ITEST.EQ.4) GO TO 32	A 226
	RHO1=RHO1*PTM/PT	A 227
	CALL FIND (P1M,RHO1,H1,S1R,T1,A1,Z1,GAME1,MU,1,1)	A 228
	GO TO 25	A 229
32	U1=U1*SQRT(PTM/PT)	A 230
	GO TO 25	A 231
33	M1=U1/A1	A 232
	QTZO=SQRT(PT/RN)*(HT-HW)/ZMIX	A 233
	IF (ITEST.NE.6.OR.ITEST.NE.7) GO TO 36	A 234
	IF (ITEST.EQ.6) GO TO 34	A 235
	CON77=PT/(RHO1*U1**2)	A 236
	IF (ABS(1.-CON7/CON77).LE..001) GO TO 35	A 237
	CON7=CON77	A 238
	IF (MMM.EQ.3) GO TO 47	A 239
	GO TO 23	A 240
34	CON66=PT/(RHO1*U1**2)	A 241
	IF (ABS(1.-CON6/CON66).LE..001) GO TO 35	A 242
	CON6=CON66	A 243
	IF (NNN.EQ.3) GO TO 47	A 244
	GO TO 16	A 245
35	IF (ABS(1.-QTZO/QTN).GE.TOLQT) GO TO 48	A 246
C		A 247
C	CALCULATING FREE-STREAM REYNOLDS NUMBER	A 248
C		A 249
36	VIS(1)=3.33E-7*TI**.739	A 250
	IF (T1.GT.950.) GO TO 37	A 251
	VIS(2)=(-.973034+.5522198*T1-1.613866E-4*T1**2)*1.E-7	A 252

# APPENDIX A - Continued

	VIS(3)=(22.99167+.5558644*TI-1.84356E-4*TI**2)*1.E-7	A 253
	VIS(4)=(19.93933+.6623589*TI-2.04096E-4*TI**2)*1.E-7	A 254
	GO TO 38	A 255
37	VIS(2)=(150.2874+.248903*TI-6.174675E-6*TI**2)*1.E-7	A 256
	VIS(3)=(163.8798+.2460075*TI-7.738745E-6*TI**2)*1.E-7	A 257
	VIS(4)=(230.3+.2559657*TI-2.264286E-6*TI**2)*1.E-7	A 258
38	W(1)=39.944	A 259
	W(2)=44.011	A 260
	W(3)=28.016	A 261
	W(4)=32.	A 262
	XMF(1)=XAR	A 263
	XMF(2)=XC02	A 264
	XMF(3)=XN2	A 265
	XMF(4)=X02	A 266
	DO 40 I=1,4	A 267
	DO 40 J=1,4	A 268
	PHI(I,J)=((1.+SQRT(VIS(1)/VIS(J)))*(W(J)/W(I))**.25)**2)/(2.8284*S	A 269
	1QRT(1.+W(I)/W(J)))	A 270
	IF (XMF(I).EQ.0.) GO TO 39	A 272
	SUM(I,J)=PHI(I,J)*XMF(J)/XMF(I)	A 273
	GO TO 40	A 274
39	SUM(I,J)=0.	A 275
40	CONTINUE	A 276
	DO 41 I=1,4	A 277
	SUM(I)=SUM(I,1)+SUM(I,2)+SUM(I,3)+SUM(I,4)	A 278
	IF (SUM(I).NE.0.) GO TO 41	A 279
	SUM(I)=1.	A 280
	VIS(I)=0.	A 281
41	CONTINUE	A 282
	VISMIX=(VIS(1)/SUMM(1))+(VIS(2)/SUMM(2))+(VIS(3)/SUMM(3))+(VIS(4)/	A 283
	1SUMM(4))	A 284
	REI=RHO1*UI/VISMIX	A 285
C		A 286
C	CALCULATING QT FROM-HOSHIZAKI, SCALA, MARVIN(NASA TR R-224)	A 287
C		A 288
	IF (XC02.LT.9) GO TO 42	A 289
	BO=(1./RN)*SQRT(2.*(PT-P1)/RHOT)	A 290
	QTHOS=5.9647E-5*SQRT(BO*RHO1)*(U1**2.69)*(1.-HW/HT)	A 291
42	IF (XAR.GT.05) GO TO 43	A 292
	QTSAL=8.4681E-6*SQRT(PT/RN)*(HT-HW)*(12.+866*MU)	A 293
43	QTAVCO=3.2675E+5*(1.+0.75*MU)*SQRT(P1/RN)*(U1/3.048E+3)**(3.909-	A 294
	10229*MU)*(P1/PT)**.535	A 295
	CON1=XAR*118.6+XC02*90.4+XN2*78.8+X02*115.5	A 296
	CON2=XAR*2.11+XC02*2.04+XN2*2.03+X02*1.838	A 297

# APPENDIX A - Continued

JTMARV=19.569640*CON1*SQRT(P1/RN)*(1.-HW/HT)*(U1/3.048E+3)**CON2										A 298
PRINT 59										A 299
PRINT 60										A 300
PRINT 55, P1,RH01,T1,H1,S1R,Z1,GAME1,A1,U1,M1,RE1										A 301
PRINT 62										A 302
PRINT 63										A 303
PRINT 55, P2,RH02,T2,H2,S2R,Z2,GAME2,A2,U2,M2										A 304
PRINT 64										A 305
PRINT 65										A 306
PRINT 55, PT,RHOT,TT,HT,STR,ZT,GAMET,AT,QTZO,HW,RN										A 307
IF (ITEST,EQ.2.OR,ITEST,EQ.5) GO TO 1										A 308
44	PRINT 67									A 309
PRINT 68										A 310
DO 45 I=1,NUMSP										A 311
PRINT 69, SPECIE(I),XMOLE(I)										A 312
45	CONTINUE									A 313
IF (ITEST,EQ.2.OR,ITEST,EQ.5) GO TO 9										A 314
GO TO 1										A 315
46	PRINT 71									A 318
GO TO 1										A 319
47	PRINT 72									A 320
PRINT 73										A 321
GO TO 36										A 322
48	PRINT 74									A 323
GO TO 1										A 324
49	STOP									A 325
C										A 326
50	FORMAT (I1I,A10//)									A 327
51	FORMAT (46H GAS MIXTURE DATA REDUCTION PROGRAM OF MILLER)									A 328
52	FORMAT (51H ALL PHYSICAL QUANTITIES IN MKS UNITS-NASA SP-7012)									A 329
53	FORMAT (//17H MEASURED INPUTS)									A 330
54	FORMAT (/107H RUN P1 U1 PT QT									A 331
55	1 RH01 WO XC02 XN2 X02 XAR)									A 332
FORMAT (11E10.3)										A 333
56	FORMAT (//38H ALL 3 ROOTS COMPLEX FOR U1 IN ITEST=6)									A 334
57	FORMAT (//40H MORE THAN 1 REAL ROOT FOR U1 IN ITEST=6)									A 335
58	FORMAT (//26H ERROR IN FALG FOR ITEST=6)									A 336
59	FORMAT (//24H FREE-STREAM CONDITIONS)									A 337
60	FORMAT (/107H P RHO T H S/R									A 338
61	Z GAME A U M NRE)									A 339
62	FORMAT (//39H STATIC CONDITIONS BEHIND NORMAL SHOCK)									A 341
63	FORMAT (/96H P RHO T H S/R									A 342
64	1 Z GAME A U M)									A 343
FORMAT (//43H STAGNATION CONDITIONS BEHIND NORMAL SHOCK)										A 344

# APPENDIX A - Continued

65	FORMAT (/106H	P	RHO	T	H	S/R	A 345
1	Z	GAME	A	QTZO	HW	RN)	A 346
67	FORMAT (/140H	MOLE FRACTIONS AT STAGNATION CONDITIONS)					A 348
68	FORMAT (/29H	SPECIE	MOLE FRACTION(/)				A 349
69	FORMAT (A10,E16.4)						A 350
71	FORMAT (/146H	ITERATIONS ON P2 EXCEED LIMIT IN ITEST=2 OR 5)					A 352
72	FORMAT (/146H	MAJOR ITERATION FOR ITEST=6 OR 7 EXCEED LIMIT)					A 353
73	FORMAT (/129H	VALUES BELOW MAY BE IN ERROR)					A 354
74	FORMAT (/137H	QTZO NOT WITHIN TOLQT OF QTM-TROUBLE)					A 355
	END						A 356-
	SUBROUTINE FIND (P,RHO,H,SR,T,AM,ZM,GAME,MU,K,L)						B 1
C							B 2
C	FIND OBTAINS THERMODYNAMIC PROPERTIES FROM SUBROUTINE ROGO WITH-						B 3
C	(1) PRESSURE AND DENSITY (K=1)						B 4
C	(2) PRESSURE AND ENTHALPY (K=2)						B 5
C	(3) PRESSURE AND ENTROPY (K=3)						B 6
C	(4) DENSITY AND ENTHALPY (K=4)						B 7
C							B 8
C							B 9
C	UPPER LIMIT ON T AS REQUIRED IN ITERATION DENOTED BY L						B 10
C	L=1 DENOTES TUP=TMAX1 FOR FREESTREAM CONDITIONS						B 11
C	L=2 DENOTES TUP=TMAX2 FOR STATIC CONDITIONS BEHIND SHOCK						B 12
C							B 13
C	IF TMAX1=0, THEN TUP=8000 DEG K						B 14
C	IF TMAX2=0, THEN TUP=16,000 DEG K						B 15
C							B 16
	DIMENSION TABT(3), TAPR(3), TABH(3), TABSR(3), TABAM(3), TABZM(3),						B 17
1	TABG(3), TABXM(3,30), TABXMO(80), TABFIT(30)						B 18
	CIMENSION TABPM(3), TABHM(3), TABSRM(3), TABTM(3), TABAMM(3), TABZ						B 19
	1MM(3), TABGM(3)						B 20
	COMMON NUMSP,JINDX,IAR,IN2,IO2,ICO2,BOZ,XAR,XN2,XO2,XCO2						B 21
	COMMON TMAX1,TMAX2,TMIN1,TMIN2						B 22
	COMMON XMOLE(30),SPECIE(30)						B 23
	REAL MU						B 24
	NN=0						B 25
	IF (K.NE.4) GO TO 10						B 26
	11=0						B 27
	MN=0						B 28
	PLOW=.01*RHO*ABS(H)						B 29
	PPP=PLow						B 30
	PUP=.51*RHO*ABS(H)						B 31
	P=(PUP-PLOW)/2.+PLOW						B 32
1	DELP=(PUP-PLOW)/2.						B 33
	IF (MN.EQ.0) GO TO 2						B 34

# APPENDIX A - Continued

	P=PUP-DELP	B 35
2	PN=P/1.01325E+5	B 36
	TLOW=0.	B 37
	IF (L.EQ.1) GO TO 3	B 38
	TUP=1.6E+4	B 39
	GO TO 4	B 40
3	TUP=R.E+3	B 41
4	MN=MN+1	B 42
	NN=0	B 43
	GO TO 16	B 44
5	IF (ABS(1.-H/HK).LE..001) GO TO 41	B 45
	IF (HK.LT.H) GO TO 6	B 46
	PUP=P	B 47
	PLOW=P-DELP	B 48
	IF (DELP.GT.PPP) GO TO 1	B 49
	TABPM(1)=PUP	B 50
	TABPM(3)=PLOW	B 51
	NNN=-2	B 52
	GO TO 7	B 53
6	PLOW=P	B 54
	PUP=P+DELP	B 55
	IF (DELP.GT.PPP) GO TO 1	B 56
	TABPM(1)=PLOW	B 57
	TABPM(3)=PUP	B 58
	NNN=2	B 59
7	TABHM(1)=HK	B 60
	TABSRM(1)=SR	B 61
	TABTM(1)=T	B 62
	TABAMM(1)=AM	B 63
	TABZMM(1)=ZM	B 64
	TABGM(1)=GAME	B 65
	DELP=(TABPM(3)-TABPM(1))/2.	B 66
	TABPM(2)=TABPM(1)+DELP	B 67
	DO 9 JK=2,3	B 68
	P=TARPM(JK)	B 69
	II=1	B 70
	GO TO 2	B 71
8	TABHM(JK)=HK	B 72
	TABSRM(JK)=SR	B 73
	TABTM(JK)=T	B 74
	TABAMM(JK)=AM	B 75
	TABZMM(JK)=ZM	B 76
	TABGM(JK)=GAME	B 77
9	CONTINUE	B 78

# APPENDIX A - Continued

	CALL FTLUP (H,SR,NNN,3,TABHM,TABSRM)	B 79
	CALL FTLUP (H,AM,NNN,3,TABHM,TABAMM)	B 80
	CALL FTLUP (H,ZM,NNN,3,TABHM,TABZMM)	B 81
	CALL FTLUP (H,T,NNN,3,TABHM,TABTM)	B 82
	CALL FTLUP (H,P,NNN,3,TABHM,TABPM)	B 83
	CALL FTLUP (H,GAME,NNN,3,TABHM,TABGM)	B 84
	GO TO 41	B 85
10	PN=P/1.01325E+5	B 86
	IF (L.EQ.2) GO TO 12	B 87
	IF (TMAX1.EQ.0.) GO TO 11	B 88
	TUP=TMAX1	B 89
	GO TO 14	B 90
11	TUP=8.E+3	B 91
	GO TO 14	B 92
12	IF (TMAX2.EQ.0.) GO TO 13	B 93
	TUP=TMAX2	B 94
	GO TO 14	B 95
13	TUP=1.6E+4	B 96
14	IF (L.EQ.2) GO TO 15	B 97
	TLOW=TMIN1	B 98
	GO TO 16	B 99
15	TLOW=TMIN2	B 100
16	T=(TUP-TLOW)/2.+TLOW	B 101
17	DELT=(TUP-TLOW)/2.	B 102
	IF (NN.EQ.0) GO TO 18	B 103
	T=TUP-DELT	B 104
18	CALL ROGO (PN,RHOA,HA,SAR,T,AM,ZM,GAME,MU)	B 105
	NN=NN+1	B 106
	IF (K.EQ.2) GO TO 23	B 107
	IF (K.EQ.3) GO TO 24	B 108
C		B 109
C	CONVERGENCE TEST FOR K=1	B 110
C		B 111
	IF (ABS(1.-RHO/RHOA),LE,.001) GO TO 36	B 112
	IF (RHO.LT.RHOA) GO TO 21	B 113
19	TUP=T	B 114
	TLOW=T-DELT	B 115
	IF (DELT.GT.250.) GO TO 17	B 116
	TABT(1)=TUP	B 117
	TABT(3)=TLOW	B 118
	IF (K.EQ.1.OR.K.EQ.4) GO TO 20	B 119
	N=-2	B 120
	GO TO 25	B 121
20	N=2	B 122

# APPENDIX A - Continued

21	GO TO 25	B 123
	TLOW=T	B 124
	TUP=T+DELT	B 125
	IF (DELT.GT.250.) GO TO 17	B 126
	TABT(1)=TLOW	B 127
	TABT(3)=TUP	B 128
	IF (K.EQ.1.OR.K.EQ.4) GO TO 22	B 129
	N=2	B 130
	GO TO 25	B 131
22	N=-2	B 132
	GO TO 25	B 133
C		B 134
C	CONVRGENCE TEST FOR K=2	B 135
C		B 136
23	IF (ABS(1.-H/HA).LE..001) GO TO 37	B 137
	IF (HA.LT.H) GO TO 21	B 138
	GO TO 19	B 139
C		B 140
C	CONVRGENCE TEST FOR K=3	B 141
		B 142
24	IF (ABS(1.-SR/SAR).LF..001) GO TO 38	B 143
	IF (SAR.LT.SR) GO TO 21	B 144
	GO TO 19	B 145
C		B 146
C	INTERPOLATION FOR DELT LESS THAN 250 DEG K	B 147
C		B 148
25	TABR(1)=RHOA	B 149
	TABH(1)=HA	B 150
	TABSR(1)=SAR	B 151
	TABAM(1)=AM	B 152
	TABZM(1)=ZM	B 153
	TABG(1)=GAME	B 154
	DO 26 J=1,NUMSP	B 155
	TABXM(1,J)=XMOLE(J)	B 156
26	CONTINUE	B 157
	DELT=(TABT(3)-TABT(1))/2.	B 158
	TABT(2)=TABT(1)+DELT	B 159
	DO 28 I=2,3	B 160
	T=TART(I)	B 161
	CALL ROGO (PN,RHOA,HA,SAR,T,AM,ZM,GAME,MU)	B 162
	DO 27 J=1,NUMSP	B 163
	TABXM(1,J)=XMOLE(J)	B 164
27	CONTINUE	B 165
	TABR(1)=RHOA	B 166



# APPENDIX A - Continued

	TABH(I)=HA	B 167
	TABSR(I)=SAR	B 168
	TABAM(I)=AM	B 169
	TABZM(I)=ZM	B 170
	TABG(I)=GAME	B 171
	CONTINUE	B 172
28	IJK=0	B 173
	DO 29 I=1,3	B 174
	DO 29 J=1,NUMSP	B 175
	IJK=IJK+1	B 176
	TABXMO(IJK)=TABXM(I,J)	B 177
29	CONTINUE	B 178
	DO 30 J=1,NUMSP	B 179
	TABFIT(J)=J	B 180
30	CONTINUE	B 181
	IY=3*NUMSP	B 182
	IF (K.EQ.2) GO TO 32	B 183
	IF (K.EQ.3) GO TO 34	B 184
	CALL FTLUP (RHO,T,N,3,TABR,TABT)	B 185
	CALL FTLUP (RHO,HK,N,3,TABR,TABH)	B 186
	CALL FTLUP (RHO,SR,N,3,TABR,TABSR)	B 187
	CALL FTLUP (RHO,AM,N,3,TABR,TABAM)	B 188
	CALL FTLUP (RHO,ZM,N,3,TABR,TABZM)	B 189
	CALL FTLUP (RHO,GAME,N,3,TABR,TABG)	B 190
	DO 31 JJ=1,NUMSP	B 191
	FIT=JJ	B 192
	CALL DISCOT (FIT,RHO,TABFIT,TABXMO,TABR,02,IY,3,XMOLE(JJ))	B 193
31	CONTINUE	B 194
	IF (K.EQ.1) GO TO 40	B 195
	IF (I1.EQ.1) GO TO 8	B 196
	GO TO 5	B 197
32	CALL FTLUP (H,T,N,3,TABH,TABT)	B 198
	CALL FTLUP (H,RHO,N,3,TABH,TABR)	B 199
	CALL FTLUP (H,SR,N,3,TABH,TABSR)	B 200
	CALL FTLUP (H,AM,N,3,TABH,TABAM)	B 201
	CALL FTLUP (H,ZM,N,3,TABH,TABZM)	B 202
	CALL FTLUP (H,GAME,N,3,TABH,TABG)	B 203
	DO 33 JJ=1,NUMSP	B 204
	FIT=JJ	B 205
	CALL DISCOT (FIT,H,TABFIT,TABXMO,TABH,02,IY,3,XMOLE(JJ))	B 206
33	CONTINUE	B 207
	GO TO 41	B 208
34	CALL FTLUP (SR,RHO,N,3,TABSR,TABR)	B 209
	CALL FTLUP (SR,H,N,3,TABSR,TABH)	B 210

# APPENDIX A - Continued

	CALL FTLUP (SR,T,N,3,TABSR,TABJ)	B 211
	CALL FTLUP (SR,AM,N,3,TABSR,TABAM)	B 212
	CALL FTLUP (SR,ZM,N,3,TABSR,TABZM)	B 213
	CALL FTLUP (SR,GAME,N,3,TABSR,TABG)	B 214
	DO 35 JJ=1,NUMSP	B 215
	FIT=JJ	B 216
	CALL DISCOT (FIT,SR,TABFIT,TABXMO,TABSR,C2,IY,3,XMOLE(JJ))	B 217
35	CONTINUE	B 218
	GO TO 41	B 219
36	IF (K.EQ.4) GO TO 39	B 220
	H=HA	B 221
	SR=SR	B 222
	GO TO 41	B 223
37	RHO=RHOA	B 224
	SR=SR	B 225
	GO TO 41	B 226
38	H=HA	B 227
	RHO=RHOA	B 228
	GO TO 41	B 229
39	HK=HA	B 230
	SR=SR	B 231
	GO TO 5	B 232
40	H=HK	B 233
41	RETURN	B 234
	END	B 235-
	SUBROUTINE ROGO (PN,RHOAN,HA,SOR,T,AM,XZ,GAMMAE,MU)	C 1
C		C 2
C	PROGRAM OF ALLISON(NASA TN D-3538) AND NEWMAN(NASA TN D-3540)	C 3
C	COMPUTES THERMOCHEMICAL EQUILIBRIUM PROPERTIES OF GAS MIXTURES	C 4
C	REQUIRES INPUTS OF P AND T	C 5
C		C 6
	COMMON NUMSP,JINDX,IAR,IN2,I02,ICO2,BOZ,XAR,XN2,XO2,XCO2	C 7
	COMMON TMAX1,TMAX2,TMIN1,TMIN2	C 8
	COMMON XMOLE(30),SPECIE(30)	C 9
	REAL NO,M,LAMB,LAMBDA,MU,NE,NEGFT,LOGNE,MASSFR,LMIN	C 10
	REAL INTENE,LGEORT,LGRORE	C 11
	INTEGER F(30),V(30,10)	C 12
	DIMENSION LB(30), M(30), DELHF(30), BETA(30), NDEFUG(30), IPIVOT(1	C 13
	10), R(10,10), SUMAY(10,1), G(30,30), E(30,30), BE(30,10), ALPHAE(3	C 14
	20,10), OMEGA(30,10), OMEGAX(30,10), XOMEG(30,4), XOMEGX(30,4), Z(3	C 15
	30), SIGMA(10), U(10), DELTA(10), GAMMA(10), XX(10), Q(30), Y(30),	C 16
	4X(30), A(30,9), HORT(30), FORT(30), NEGFT(30), PI(9,2), XPRIME(30	C 17
	5), MASSFR(30), CAPX(50), YINT(30,5), CSUBP(30), PSI(30,2), CON(10,	C 18
	62), OXDT(30), RR(10,10), O(10,10)	C 19

# APPENDIX A - Continued

	DIMENSION HEPG(30), OMSFRDT(30)	C 20
	H=6.62517E-27	C 21
	XK=1.38044E-16	C 22
	PREF=1.013250E+6	C 23
	NO=6.02322E+23	C 24
	C=2.99793E+10	C 25
	IF (ROZ.EQ.1.) GO TO 3	C 26
	BOZ=1.	C 27
	EA=1.E-12	C 28
	ER=1.E-1	C 29
	DO 2 I=1,NUMSP	C 30
	READ (5,74) SPECIE(I),LB(I),F(I),NDEBUG(I),M(I),DELHF(I),BETA(I)	C 31
	IL=LR(I)	C 32
C	IF NDEBUG EQUALS 0, DEBUG	C 33
	READ (5,75) (G(I,L),F(I,L),L=1,IL)	C 34
	IF (F(I),EQ.0) GO TO 2	C 35
	IF (F(I),EQ.2) GO TO 1	C 36
	READ (5,76) (BE(I,L),ALPHA(I,L),OMEGA(I,L),OMEGAX(I,L),V(I,L),L=1	C 37
	1,IL)	C 38
	GO TO 2	C 39
1	READ (5,75) BE(I,1),ALPHA(I,1)	C 40
	READ (5,75) (XOMEG(I,LW),XOMEGX(I,LW),LW=1,4)	C 41
2	CONTINUE	C 42
	READ (5,77) (A(I,J),J=1,JNDX),I=1,NUMSP	C 43
3	DO 4 I=1,NUMSP	C 44
4	YINT(I,1)=1.E-20	C 45
	YINT(I02,1)=1.E-5	C 46
	IF (XAR.EQ.0.) GO TO 5	C 47
	YINT(IAR,1)=XAR/MU	C 48
5	IF (XN2.EQ.0.) GO TO 6	C 49
	YINT(IN2,1)=XN2/MU	C 50
6	IF (X02.EQ.0.) GO TO 7	C 51
	YINT(I02,1)=X02/MU	C 52
7	IF (XC02.EQ.0.) GO TO 8	C 53
	YINT(IC02,1)=XC02/MU	C 54
8	RH00=PREF*MU/(NO*XK*273.15)	C 55
	DO 9 I=1,NUMSP	C 56
9	IF (YINT(I,1).EQ.0.) YINT(I,1)=1.E-20	C 57
	AO=SQRT(1.4*(PREF/RH00))	C 58
	NUMT=NCAPX=1	C 59
	LEEB0B=INDEP=0	C 60
	IF (INDEP.NE.0) GO TO 11	C 61
	DO 10 KP=1,NCAPX	C 62
10	CAPX(KP)=ALOG10(PN)	C 63

# APPENDIX A - Continued

11	DO 73 KI=1,NUMT	C 64
	IF (LEEB0B.EQ.1) PUNCH 81, T	C 65
	NY=1	C 66
	PART=H*C/(XK*T)	C 67
	DO 19 I=1,NUMSP	C 68
	IL=LR(I)	C 69
	IF (F(I).EQ.1) GO TO 13	C 70
	IF (F(I).EQ.2) GO TO 16	C 71
	QSUM=0.	C 72
	FQSUM=0.	C 73
	SQSUM=0.	C 74
	DO 12 L=1,IL	C 75
	Z(L)=PART*E(I,L)	C 76
	GEZ=G(I,L)*EXP(-Z(L))	C 77
	QSUM=QSUM+GEZ	C 78
	FQSUM=FQSUM+GEZ*Z(L)	C 79
12	SQSUM=SQSUM+(Z(L)-2.)*GEZ*Z(L)	C 80
	FQSUM=FQSUM/T	C 81
	SQSUM=SQSUM/T**2	C 82
	QI=(M(I)*T*.32807618)**1.5*QSUM*.13623883*T	C 83
	GO TO 18	C 84
13	QSUM=0.	C 85
	FQSUM=0.	C 86
	SQSUM=0.	C 87
	DO 15 L=1,IL	C 88
	Z(L)=PART*E(I,L)	C 89
	SIGMA(L)=PART*(BE(I,L)-.5*ALPHA(I,L))	C 90
	U(L)=PART*(OMEGA(I,L)-2.*OMEGAX(I,L))	C 91
	DELTA(L)=ALPHA(I,L)*1./(BE(I,L)-.5*ALPHA(I,L))	C 92
	GAMMA(L)=(BE(I,L)/OMEGA(I,L))**2*1./(1.-.5*ALPHA(I,L)/BE(I,L))	C 93
	XX(L)=OMEGAX(I,L)/(OMEGA(I,L)-2.*OMEGAX(I,L))	C 94
	THREF=0.	C 95
	FOUR=0.	C 96
	FIVE=0.	C 97
	NV=V(I,L)+1	C 98
	DO 14 IV=1,NV	C 99
	W=IV-1	C 100
	CC=(1.-W*DELTA(L))	C 101
	AA=SIGMA(L)*CC	C 102
	BB=U(L)*(W-XX(L)*W*(W-1.))	C 103
	ONE1=1./AA+8.*GAMMA(L)/(AA**2*CC)+.33333333+AA/12.	C 104
	TWO2=1./AA+16.*GAMMA(L)/(AA**2*CC)-AA/12.-384.*GAMMA(L)**2/(AA**3*	C 105
	1CC**2)	C 106
	THREE=THREE+ONE1*EXP(-BB)	C 107

# APPENDIX A - Continued

	FOUR=FOUR+(BB*ONE1+TW02)*EXP(-BB)	C 108
14	FIVE=FIVE+((BB**2*ONE1+2.*BB*TW02+GAMMA(L)/(AA**2*CC))*(48.-3456.*G	C 109
	IAMMA(L)/(AA*CC)+46080.*GAMMA(L)**2/(AA**2*CC**2))+2./AA)*EXP(-BB))	C 110
	GEZ=G(I,L)*EXP(-Z(L))	C 111
	Q(L)=THREE/BETA(I)*GFZ	C 112
	QSUM=QSUM+Q(L)	C 113
	FPQSUM=FPQSUM+(FOUR+THREE*Z(L))*GEZ	C 114
15	SPQSUM=SPQSUM+(Z(L)*(Z(L)-2.)*THREE+2.*(Z(L)-1.)*FOUR+FIVE)*GEZ	C 115
	FPQSUM=FPQSUM/(T*BETA(I))	C 116
	SPQSUM=SPQSUM/(T**2*RETA(I))	C 117
	Q1=(M(I)*T*.32807618)**1.5*QSUM*.13623883*T	C 118
	GO TO 18	C 119
16	SIGMA(I)=PART*(BE(I,1)-.5*ALPHA(I,1))	C 120
	PROD=1.	C 121
	SUM1=0.	C 122
	SUM2=0.	C 123
	DO 17 LW=1,4	C 124
	U(LW)=PART*(XOMEG(I,LW)-XOMEGX(I,LW))	C 125
	PROD=PROD*(1.-EXP(-U(LW)))	C 126
	BTM=EXP(U(LW))-1.	C 127
	SUM1=SUM1+U(LW)/BTM	C 128
17	SUM2=SUM2+U(LW)**2*EXP(U(LW))/BTM**2	C 129
	QSUM=G(I,1)/(BETA(I)*SIGMA(I)*PROD)	C 130
	FPQSUM=(1.+SUM1)*QSUM/T	C 131
	SPQSUM=(SUM1**2+SUM2)*QSUM/T**2	C 132
	Q1=(M(I)*T*.32807618)**1.5*QSUM*.13623883*T	C 133
18	HORT(I)=2.5+T/QSUM*FPQSUM+DELHF(I)/(NO*XK*T)	C 134
	HEPG(I)=HORT(I)*NO*XK*T/M(I)	C 135
	FORT(I)=DELHF(I)/(NO*XK*T)-ALOG(Q1)	C 136
	NEGFRT(I)=-FORT(I)	C 137
19	CSUBP(I)=2.5+2.*T/QSUM*FPQSUM-(T*FPQSUM/QSUM)**2+T**2*SPQSUM/QSUM	C 138
	IF (LEEB0B.EQ.1) PUNCH 81, (CSUBP(I),HORT(I),I=1,NUMSP)	C 139
	NNN=1	C 140
	DO 72 KP=1,NCAPX	C 141
	IF (INDEP.EQ.2) SAVERHO=CAPX(KP)	C 142
	P=(10.**CAPX(KP))*PREF	C 143
	POPO=P/PREF	C 144
	DO 20 I=1,NUMSP	C 145
20	Y(I)=YINT(I,NY)	C 146
	NUMIT=0	C 147
	NUMITF=0	C 148
	MM=JINDX+1	C 149
	DO 22 J=1,JINDX	C 150
	O(J,MM)=0.	C 151

# APPENDIX A - Continued

	DO 21 I=1,NUMSP	C 152
21	O(J,MM)=O(J,MM)+A(I,J)*Y(I)	C 153
	O(MM,J)=O(J,MM)	C 154
22	CONTINUE	C 155
	O(MM,MM)=O.	C 156
23	CONTINUE	C 157
	YBAR=Y(I)	C 158
	NUMIT=NUMIT+1	C 159
	IF (NUMIT.EQ.201) GO TO 59	C 160
	DO 24 I=2,NUMSP	C 161
24	YBAR=YBAR+Y(I)	C 162
	IF (INDEP.EQ.2) P=NO* XK*T*YBAR*CAPX(KP)	C 163
	DO 26 K=1,JINDX	C 164
	R(I,K)=O.	C 165
	DO 25 I=1,NUMSP	C 166
25	R(I,K)=R(I,K)+A(I,I)*A(I,K)*Y(I)	C 167
26	CONTINUE	C 168
	ICOUNT=1	C 169
	JJ=2	C 170
	DO 30 J=JJ,JINDX	C 171
	DO 28 K=J,JINDX	C 172
	R(J,K)=O.	C 173
	DO 27 I=1,NUMSP	C 174
27	R(J,K)=R(J,K)+A(I,J)*A(I,K)*Y(I)	C 175
28	CONTINUE	C 176
	DO 29 K=1,ICOUNT	C 177
29	R(J,K)=R(K,J),	C 178
	ICOUNT=ICOUNT+1	C 179
30	JJ=1+ICOUNT	C 180
	DO 31 J=1,MM	C 181
	R(J,MM)=O(J,MM)	C 182
31	R(MM,J)=O(J,MM)	C 183
	DO 32 J=1,MM	C 184
	DO 32 K=1,MM	C 185
32	RR(J,K)=R(J,K)	C 186
	PYBAR=PRF*YBAR	C 187
	DO 34 J=1,JINDX	C 188
	SUMAY(J,I)=O.	C 189
	DO 33 I=1,NUMSP	C 190
	THIS=PY(I)/PYBAR	C 191
	IF (THIS.LE.O.) GO TO 33	C 192
	SUMAY(J,I)=SUMAY(J,I)+A(I,J)*Y(I)*(FORT(I)+ALOG(THIS))	C 193
33	CONTINUE	C 194
34	CONTINUE	C 195

# APPENDIX A - Continued

	SUMAY(MM,1)=0.	C 196
	DO 35 I=1,NUMSP	C 197
	THIS=P*Y(I)/PYBAR	C 198
	IF (THIS.LE.0.) GO TO 35	C 199
	SUMAY(MM,1)=SUMAY(MM,1)+Y(I)*(FORT(I)+ALOG(THIS))	C 200
35	CONTINUE	C 201
	MN=1	C 202
	NMAX=10	C 203
	CALL SIMEQ (R,MM,SUMAY,MN,DETERM,PIPOT,NMAX,ISCALE)	C 204
	DO 36 J=1,JINDX	C 205
36	PI(J,1)=SUMAY(J,1)	C 206
	U=SUMAY(MM,1)	C 207
	LMIN=1.	C 208
	LCOUNT=0	C 209
	DO 43 I=1,NUMSP	C 210
	API=0.	C 211
	DO 37 J=1,JINDX	C 212
37	API=API+A(I,J)*PI(J,1)	C 213
	THIS=P*Y(I)/PYBAR	C 214
	IF (THIS.LE.0.) GO TO 38	C 215
	X(I)=Y(I)*(NEGFRT(I)-ALOG(THIS)+U+1.*API)	C 216
	GO TO 39	C 217
38	X(I)=0.	C 218
39	IF (X(I)) 40,42,43	C 219
40	LAMB=-Y(I)/(X(I)-Y(I))	C 220
	IF (LAMB.GT.0.) GO TO 41	C 221
	Y(I)=0.	C 222
	GO TO 23	C 223
41	LCOUNT=1	C 224
	LMIN=AMIN1(LMIN,LAMB)	C 225.
	GO TO 43	C 226
42	IF (Y(I).EQ.0.) GO TO 43	C 227
	LCOUNT=1	C 228
	LAMB=1.	C 229
	LMIN=AMIN1(LMIN,LAMB)	C 230
43	CONTINUE	C 233
	IF (LCOUNT.EQ.0) GO TO 45	C 234
	LAMBDA=.9999999999999999*LMIN	C 235
	DO 44 I=1,NUMSP	C 236
	Y(I)=(1.-LAMBDA)*Y(I)+LAMBDA*X(I)	C 237
44	IF (Y(I).LT.1.E-100) Y(I)=0.	C 238
	GO TO 23	C 239
45	DO 46 I=1,NUMSP	C 240
	IF (Y(I).EQ.0.) GO TO 46	C 241

# APPENDIX A - Continued

46	IF (ABS(X(I)-Y(I))/Y(I)).GE.ER.OR.ABS(X(I)-Y(I)).GE.EA) GO TO 47	C 242
	CONTINUE	C 243
47	GO TO 54	C 244
	XBAR=0.	C 245
	LAMBDA=1.	C 246
	LASTCT=0	C 247
48	DO 49 I=1,NUMSP	C 248
	XPRIME(I)=(1.-LAMBDA)*Y(I)+LAMBDA*X(I)	C 249
49	XBAR=XBAR+XPRIME(I)	C 250
	DFLAMB=0.	C 251
	DO 50 I=1,NUMSP	C 252
	THIS=P*XPRIME(I)/(PRFF*XBAR)	C 253
	IF (THIS.LE.1.E-38) GO TO 50	C 254
50	DFLAMB=DFLAMB+(X(I)-Y(I))*(FORT(I)+ALOG(THIS))	C 255
	CONTINUE	C 256
	IF (DFLAMB.GT.0.) GO TO 53	C 257
51	DO 52 I=1,NUMSP	C 258
52	Y(I)=XPRIME(I)	C 259
	GO TO 23	C 260
53	LASTCT=LASTCT+1	C 261
	IF (LASTCT.EQ.4) GO TO 51	C 262
	LAMBDA=.9*LAMBDA	C 263
	XBAR=0.	C 264
	GO TO 48	C 265
54	IF (NUMITF.EQ.1) GO TO 56	C 266
	NUMITO=0	C 267
	IF (INDEP.NE.2) GO TO 56	C 268
	NUMITF=1	C 269
	NUMITO=NUMIT	C 270
	INDEP=1	C 271
55	DO 55 I=1,NUMSP	C 272
	Y(I)=X(I)	C 273
56	GO TO 23	C 274
	XBAR=0.	C 275
	ONE=0.	C 276
	TWO=0.	C 277
	DO 57 I=1,NUMSP	C 278
	XBAR=XBAR+X(I)	C 279
	ONE=ONE+X(I)*HOUT(I)	C 280
	MASSFR(I)=X(I)*M(I)	C 281
	IF (Y(I).EQ.0.) GO TO 57	C 282
	TWO=TWO+X(I)*(FORT(I)+ALOG(X(I)))	C 283
57	CONTINUE	C 284
	RECIPZ=1./(MU*XBAR)	C 285



# APPENDIX A - Continued

	IF (NUMITF.EQ.1) CAPX(KP)=ALOG10(P/PREF)	C 286
	IF (NUMITF.EQ.1) INDFP=2	C 287
	CAPU=CAPX(KP)+ALOG10(RECIPZ*273.15/T)	C 288
	CHORT=MU*ONE	C 289
	SOR=CHORT-MU*(XBAR*ALOG(P/(PREF*XBAR))+TWO)	C 290
	RHO=P/(XBAR*NO*XK*T)	C 291
	NE=X(1)*RHO*NO	C 292
	IF (X(1).GT.10.**-20) GO TO 58	C 293
	LOGNF=-0.	C 294
	GO TO 60	C 295
58	LOGNF=ALOG10(NE)	C 296
	GO TO 60	C 297
59	WRITE (6,78) P	C 298
	GO TO 72	C 299
60	CONTINUE	C 300
	DO 62 I=1,NUMSP	C 301
	TEST=X(I)*P/(XBAR*PRFF)	C 302
	IF (TEST.LT.10.**(-20)) GO TO 61	C 303
	PSI(I,1)=X(I)/T*(HORT(I)-FORT(I)-ALOG(TEST))	C 304
	PSI(I,2)=-X(I)	C 305
	GO TO 62	C 306
61	PSI(I,1)=0.	C 307
	PSI(I,2)=0.	C 308
62	CONTINUE	C 309
	DO 64 J=1,JINDX	C 310
	CON(J,1)=A(I,J)*PSI(I,1)	C 311
	CON(J,2)=A(I,J)*PSI(I,2)	C 312
	DO 63 I=2,NUMSP	C 313
	CON(J,1)=CON(J,1)+A(I,J)*PSI(I,1)	C 314
63	CON(J,2)=CON(J,2)+A(I,J)*PSI(I,2)	C 315
64	CONTINUE	C 316
	CON(MM,1)=PSI(I,1)	C 317
	CON(MM,2)=PSI(I,2)	C 318
	DO 65 I=2,NUMSP	C 319
	CON(MM,1)=CON(MM,1)+PSI(I,1)	C 320
65	CON(MM,2)=CON(MM,2)+PSI(I,2)	C 321
	NC=2	C 322
	CALL SIMEQ (RR,MM,CON,NC,DETERM,PIVOT,NMAX,ISCALE)	C 323
	DO 66 J=1,MM	C 324
	PI(J,1)=CON(J,1)	C 325
66	PI(J,2)=CON(J,2)	C 326
	DHDT=0.	C 327
	DO 68 I=1,NUMSP	C 328
	SUMAP=A(I,1)*PI(I,1)	C 329

# APPENDIX A - Continued

	DO 67 J=2,JINDEX	C 330
67	SUMAP=SUMAP+A(I,J)*PI(J,I)	C 331
	DXDT(I)=PSI(I,I)-X(I)*PI(MM,I)+SUMAP	C 332
	DMSFRDT(I)=M(I)*DXDT(I)	C 333
68	DHDT=DHDT+(X(I)*CSUBP(I)+T*HORT(I)*DXDT(I))	C 334
	DRHONT=T*PI(MM,I)-I.	C 335
	DRHONP=I.+PI(MM,2)	C 336
	CPOR=MU*DHDT	C 337
	XZ=XRAR*MU	C 338
	CVOR=CPOR-DRHONT**2/DRHONP*XZ	C 339
	XGAMMA=CPOR/CPOR	C 340
	GAMMAE=XGAMMA/DRHONP	C 341
	RHOR=1./(10.**CAPU)	C 342
	HPGRAM=CHORT*NO*XK*T/MU	C 343
	TEST=(GAMMAE/1.4*P/PREF*RHOR)	C 344
	IF (TEST.LE.0.) WRITE (6,80) CAPX(KP),CAPU,XZ,CHORT,SOR,LOGNE,DRHO	C 345
	1DT,DRHONP,CPOR,CPOR,XGAMMA,GAMMAE,AAO	C 346
	AAO=SORT(TEST)	C 347
	AM=AAO*AAO*.01	C 348
	RHOAN=(10.**CAPU)*RHON*1.E+3	C 349
	HA=CHORT*8.31469E+3*T/MU	C 350
	INTENE=((CHORT-XZ)*NO*XK*T+3.93146E+12)/MU	C 351
	GAMBAR=(INTENE+(P/RHO))/INTENE	C 352
	EORTO=INTENE*28.9672/(NO*XK*273.15)	C 353
	LGEORT=ALOG10(EORTO)	C 354
	RORHOE=RHO/1.2923366E-3	C 355
	LGROR=ALOG10(RORHOE)	C 356
	DO 69 I=1,NUMSP	C 357
69	XMOLE(I)=MASSFR(I)*MU/(XZ*M(I))	C 358
	IF (NNN.EQ.10) GO TO 70	C 359
	GO TO 71	C 360
70	WRITE (6,79)	C 361
	NNN=0	C 362
71	NNN=NNN+1	C 363
	IF (INDEP.EQ.2) CAPX(KP)=SAVERHO	C 364
	IF (LEEBOB.EQ.0) GO TO 72	C 365
	IF (KP.EQ.1) PUNCH 82, NCAPX	C 366
	PUNCH 81, POPO,CPOR	C 367
	PUNCH 83, (XMOLE(I),I=1,NUMSP)	C 368
72	CONTINUE	C 369
73	CONTINUE	C 370
	RETURN	C 371
C		
74	FORMAT (A6,3I5,3E14.8)	C 372
		C 373

## APPENDIX A – Concluded

75	FORMAT (5E14.8)	C 374
76	FORMAT (4E14.8,15)	C 375
77	FORMAT (15E5.0)	C 376
78	FORMAT (1X,2HP=E15.8,2X,28H200 ITERATIONS-NONCONVERGENT)	C 377
79	FORMAT (/)	C 378
80	FORMAT (/F9.4,F10.4,F9.4,F11.4,F10.4,F9.3,F10.3,F10.3,F10.3,	C 379
	1F8.3,F8.3,F9.3)	C 380
81	FORMAT (2E16.8)	C 381
82	FORMAT (15)	C 382
83	FORMAT (5E16.8)	C 383
	END	C 384

## APPENDIX B

### COMPUTER PROGRAM INPUTS

The inputs necessary to utilize the included computer program are presented in the following table:

Program (FORTRAN) symbol	Description
ITEST	Data reduction procedure to be used
RUN	Facility test number
TØLPT	Convergence criteria for iteration involving $p_t$
TØLQT	Convergence criteria for iteration involving $\dot{q}_t$
TWE	$T_w$
RN	$r_g$
PCØ2	Measured partial pressure of CO <sub>2</sub>
PN2	Measured partial pressure of N <sub>2</sub>
PØ2	Measured partial pressure of O <sub>2</sub>
PAR	Measured partial pressure of Ar
PMIX	Measured pressure of mixture
P1M	$(p_1)_m$
PTM	$(p_t)_m$
QTM	$(\dot{q}_t)_m$
RHØ1M	$(\rho_1)_m$
U1M	$(U_1)_m$
TMAX1	Maximum $T_1$ expected
TMAX2	Maximum $T_t$ expected
TMIN1	Minimum $T_1$ expected
TMIN2	Minimum $T_2$ expected
NUMSP	Number of species considered
JINDEX	Number of components considered
IAR	Position in species array of Ar
IN2	Position in species array of N <sub>2</sub>
IØ2	Position in species array of O <sub>2</sub>
ICØ2	Position in species array of CO <sub>2</sub>

## APPENDIX B – Continued

The FORTRAN NAMELIST capability is used for the input data with INP as the NAMELIST name. A sample listing of the input cards for the 26-species air test case (ITEST = 3) is as follows:

```
$INP ITEST=3,RUN=1,P1M=1040,U1M=6100,RH01M=.00485,RN=.0127,PMIX=1,
PCO2=.00033,PN2=.78084,P02=.20946,PAR=.00937,NUMSP=26,JINDX=5,IAR=2,
IN2=8,I02=14,ICO2=26$
```

The units for the inputs which are physical quantities are given in the section entitled "SYMBOLS." In using a specific ITEST, only those three measured inputs (combinations of P1M, U1M, RH01M, PTM, and QTM) associated with this ITEST need be included. (The required measured inputs corresponding to a specific ITEST are given in the section entitled "Procedures for Determining Free-Stream and Postshock Conditions.") It should be noted that the condition

$$PMIX = PAR + PN2 + P02 + PC02$$

must be satisfied. If Ar, N<sub>2</sub>, O<sub>2</sub>, or CO<sub>2</sub> is not included in the test gas, then the partial pressure (PAR, PN<sub>2</sub>, P0<sub>2</sub>, and PC0<sub>2</sub>, respectively) need not be included as input. The IAR, IN<sub>2</sub>, I0<sub>2</sub>, and IC0<sub>2</sub> need be included as input only if Ar, N<sub>2</sub>, O<sub>2</sub>, or CO<sub>2</sub>, respectively, is included in the species deck. (The computer cards containing the thermodynamic data for the various species are denoted as the species deck and are discussed subsequently.) The following table presents assigned values given to input quantities when these quantities are omitted from INP:

Input quantity omitted (program symbol)	Assigned value
T0LPT	0.001
T0LQT	0.005
TWE	300
RN	0.01
TMAX1	8 000
TMAX2	16 000
TMIN1	0
TMIN2	0

## APPENDIX B – Continued

The 26 species and five components considered are as follows:

### Species:

$e^-$	O	C
Ar	$O^+$	$C^+$
$Ar^+$	$O^{++}$	$C^{++}$
$Ar^{++}$	$O^-$	$C^-$
N	$O_2$	CO
$N^+$	$O_2^+$	$CO^+$
$N^{++}$	$O_2^-$	CN
$N_2$	NO	$CO_2$
$N_2^+$	$NO^+$	

### Components:

$e^-$   
 Ar  
 N  
 O  
 C

The thermodynamic data for these species, which are tabulated in reference 2, are read into the computer program from cards. A listing of these cards for all 26 species is as follows:

# APPENDIX B – Continued

E-	1	0	0	54847000-03	00000000+00	00000000+00
20000000+01				00000000+00		
A	30	0	0	39944000+02	00000000+00	00000000+00
10000000+01				00000000+00	50000000+01	93144000+05
93751000+05				10000000+01	94554000+05	30000000+01
30000000+01				10410200+06	12000000+02	10550000+06
10615000+06				10000000+01	10705400+06	80000000+01
40000000+01				10800000+06	40000000+01	11128000+06
11175000+06				80000000+01	11290000+06	20000000+02
16000000+02				11475000+06	80000000+01	11500000+06
11666000+06				12000000+02	11696000+06	80000000+01
10000000+01				11756300+06	16000000+02	11853000+06
11930000+06				56000000+02	12025000+06	20000000+02
32000000+02				12175000+06	36000000+02	12220000+06
12270000+06				20000000+02	12350000+06	28000000+02
A+	30	0	0	39943000+02	15202350+14	00000000+00
60000000+01				00000000+00	20000000+01	10872300+06
13240000+06				12000000+02	13480000+06	60000000+01
28000000+02				14270000+06	60000000+01	14520000+06
14765000+06				10000000+02	14875000+06	10000000+02
12000000+02				15516000+06	30000000+02	15830000+06
16100000+06				20000000+01	16730900+06	14000000+02
26000000+02				17300000+06	38000000+02	17480000+06
17970000+06				40000000+02	18300000+06	60000000+02
62000000+02				19020000+06	34000000+02	19220000+06
19400000+06				84000000+02	19600000+06	48000000+02
18000000+02				20500000+06	60000000+01	20859300+06
21000000+06				50000000+02	21500000+06	70000000+02
A++	30	0	0	39943000+02	41851700+14	00000000+00
50000000+01				00000000+00	30000000+01	11120000+04
15700000+04				50000000+01	14010000+05	10000000+01
90000000+01				11440000+06	10000000+02	12800000+06
14465000+06				15000000+02	15695000+06	50000000+01
15000000+02				18200000+06	75000000+02	18950000+06
19660000+06				50000000+01	20000000+06	18000000+02
21000000+02				20830000+06	27000000+02	21080000+06
21450000+06				46000000+02	22450000+06	90000000+01
50000000+01				23500000+06	26000000+02	24000000+06
24603600+06				91000000+02	25100000+06	24000000+02
12700000+03				27000000+06	12100000+03	27850000+06
28200000+06				11100000+03	28600000+06	52400000+03
N	30	0	0	14008000+02	47072900+13	00000000+00
40000000+01				00000000+00	10000000+02	19225000+05
28840000+05				12000000+02	83330000+05	60000000+01

# APPENDIX B – Continued

12000000+02	88140000+05	20000000+01	93582000+05	20000000+02
94800000+05	12000000+02	95500000+05	40000000+01	96752000+05
10000000+02	96810000+05	60000000+01	97800000+05	10000000+02
99660000+05	18000000+02	10400000+06	34000000+02	10470000+06
56000000+02	10500000+06	22000000+02	10660000+06	16000000+02
10720000+06	16000000+02	10760000+06	54000000+02	10960000+06
12000000+02	10986000+06	10600000+03	11035000+06	13200000+03
11160000+06	13600000+03	11220000+06	60000000+01	11231000+06
68000000+02	11282000+06	30000000+02	11291000+06	20000000+01
11360000+06	10000000+02	11390000+06	14000000+02	11700000+06
N+ 30 0 0 14007000+02 18726070+14 00000000+00				
90000000+01	00000000+00	50000000+01	15316000+05	10000000+01
32687000+05	50000000+01	47168000+05	15000000+02	92245000+05
90000000+01	10922000+06	50000000+01	14418900+06	12000000+02
14900000+06	30000000+01	15513000+06	30000000+01	16461200+06
18000000+02	16665000+06	30000000+01	16889300+06	90000000+01
17062000+06	50000000+01	17421200+06	10000000+01	17827400+06
41000000+02	18709000+06	16000000+02	18910000+06	30000000+01
19012100+06	12000000+02	19720000+06	30000000+02	20300000+06
21000000+02	20570000+06	15300000+03	21050000+06	12000000+02
21482800+06	12000000+02	21800000+06	54600000+03	22050000+06
37000000+02	22300000+06	15000000+02	22600000+06	15000000+02
22800000+06	14000000+02	23030000+06	50000000+01	23425000+06
N++ 30 0 0 14007000+02 47288300+14 00000000+00				
60000000+01	00000000+00	12000000+02	57280000+05	10000000+02
10102600+06	20000000+01	13104400+06	60000000+01	14592000+06
40000000+01	18680200+06	10000000+02	20307800+06	20000000+01
22130200+06	60000000+01	23040700+06	60000000+01	24569000+06
10000000+02	26724200+06	12000000+02	28765000+06	60000000+01
29721000+06	20000000+01	30108800+06	32000000+02	31050000+06
40000000+01	31422400+06	22000000+02	31755000+06	14000000+02
32028800+06	10000000+02	32104000+06	30000000+02	32900000+06
22000000+02	33330000+06	22000000+02	33629000+06	20000000+02
33955000+06	48000000+02	34300000+06	24000000+02	34800000+06
32000000+02	36400000+06	12000000+02	36862000+06	22000000+02
37400000+06	52000000+02	37900000+06	20000000+01	38070000+06
N2 6 1 0 28016000+02 00000000+00 20000000+01				
10000000+01	00000000+00	30000000+01	49757000+05	60000000+01
59314000+05	20000000+01	68953000+05	10000000+01	70700000+05
60000000+01	87984000+05			
19980000+01	17000000+01	23580700+04	14190000+02	33
14400000+01	13000000+01	14603700+04	13890000+02	26
16380000+01	18400000+01	17341100+04	14470000+02	29
16182000+01	18300000+01	16937000+04	13830000+02	30



# APPENDIX B – Continued

14800000+01	16400000-01	15300000+04	12000000+02	31
18258000+01	19700000-01	20351000+04	17080000+02	29
N2+ 4 1	0 28015000+02	15033360+14	20000000+01	
20000000+01	00000000+00	40000000+01	90200000+04	20000000+01
25570000+05	20000000+01	64550000+05		
19322000+01	20200000-01	22072300+04	16220000+02	32
17220000+01	18000000-01	19028400+04	14910000+02	31
20830000+01	19500000-01	24198400+04	23190000+02	25
16500000+01	50000000-01	20500000+04	14920000+02	30
0 28 0	0 16000000+02	24674100+13	00000000+00	
50000000+01	00000000+00	30000000+01	15900000+03	10000000+01
22700000+03	50000000+01	15868000+05	10000000+01	33792000+05
50000000+01	73768000+05	30000000+01	76795000+05	15000000+02
86630000+05	90000000+01	88630000+05	50000000+01	95476000+05
30000000+01	96226000+05	36000000+02	97420000+05	15000000+02
97488000+05	15000000+02	99094000+05	90000000+01	99680000+05
90000000+01	10000000+06	15000000+02	10114000+06	50000000+01
10211600+06	30000000+01	10241200+06	50000000+01	10266200+06
25000000+02	10286500+06	15000000+02	10290800+06	90000000+01
10386900+06	15000000+02	10400000+06	25000000+02	10538500+06
15000000+02	10540800+06	56000000+02	10600000+06	56000000+02
10700000+06				
0+ 30 0	0 15999000+02	15603890+14	00000000+00	
40000000+01	00000000+00	10000000+02	26820000+05	60000000+01
40465000+05	12000000+02	12000000+06	10000000+02	16599000+06
12000000+02	18540000+06	60000000+01	18900000+06	20000000+01
19571000+06	20000000+01	20394200+06	42000000+02	20760000+06
26000000+02	21280000+06	20000000+01	22685100+06	24000000+02
23000000+06	80000000+02	23270000+06	16000000+02	23390000+06
18000000+02	23960000+06	40000000+02	24550000+06	20000000+02
24800000+06	60000000+01	25030000+06	32000000+02	25190000+06
44000000+02	25400000+06	84000000+02	25550000+06	11600000+03
25600000+06	18000000+02	25810000+06	10000000+02	25930000+06
72000000+02	26150000+06	16600000+03	26550000+06	13400000+03
27000000+06	14200000+03	27650000+06	24000000+02	28300000+06
0++ 30 0	0 15999000+02	49479960+14	00000000+00	
90000000+01	00000000+00	50000000+01	20271000+05	10000000+01
43184000+05	50000000+01	60312000+05	15000000+02	12005000+06
90000000+01	14238300+06	50000000+01	18704900+06	30000000+01
19708700+06	30000000+01	21045900+06	12000000+02	27000000+06
90000000+01	28390000+06	26000000+02	29400000+06	14000000+02
30300000+06	10000000+01	31380100+06	50000000+02	32700000+06
10000000+02	33200000+06	15000000+02	33870000+06	10000000+01
34330300+06	90000000+01	35020000+06	12000000+02	35750000+06

# APPENDIX B - Continued

46000000+02	36500000+06	48000000+02	37050000+06	15800000+03
38000000+06	62000000+02	39400000+06	90000000+02	39800000+06
55800000+03	40340000+06	72000000+02	42500000+06	31100000+03
43000000+06	48000000+02	43800000+06	15000000+02	44271000+06
0- 1 0	0 16001000+02	10541000+13	00000000+00	
60000000+01	00000000+00			
02 6 1	0 32000000+02	00000000+00	20000000+01	
30000000+01	00000000+00	20000000+01	78824000+04	10000000+01
13120900+05	30000000+01	35713000+05	10000000+01	36212700+05
30000000+01	49363100+05			
14457000+01	15800000-01	15803600+04	12070000+02	26
14264000+01	17100000-01	15093000+04	12900000+02	29
14004000+01	18200000-01	14326900+04	13950000+02	25
10500000+01	35700000-01	81900000+03	22500000+02	8
82600000+00	20500000-01	65040000+03	17030000+02	9
81900000+00	11000000-01	70036000+03	80000000+01	21
02+ 4 1	0 31999000+02	11628080+14	20000000+01	
40000000+01	00000000+00	80000000+01	31500000+05	40000000+01
38300000+05	40000000+01	48100000+05		
16722000+01	19800000-01	18764000+04	16530000+02	28
11047000+01	15800000-01	10356900+04	10390000+02	24
10617000+01	19100000-01	90000000+03	13400000+02	16
12873000+01	22100000-01	11967700+04	17090000+02	17
02- 3 1	0 32001000+02	-96232000+12	20000000+01	
40000000+01	00000000+00	40000000+01	13400000+05	40000000+01
24200000+05				
12000000+01	16000000-01	13000000+04	14000000+02	29
97000000+00	17000000-01	99000000+03	15000000+02	16
92000000+00	27000000-01	56000000+03	13000000+02	10
NO 8 1	0 30008000+02	89860000+12	10000000+01	
20000000+01	00000000+00	20000000+01	12090000+03	20000000+01
44200000+05	40000000+01	45440000+05	20000000+01	53290000+05
40000000+01	52376000+05	20000000+01	60860000+05	40000000+01
60020000+05				
17046000+01	17800000-01	19040300+04	13970000+02	27
17046000+01	17800000-01	19036800+04	13970000+02	33
19972000+01	19300000-01	23748000+04	16460000+02	35
11260000+01	15200000-01	10376800+04	76030000+01	33
20026000+01	21800000-01	23239000+04	22885000+02	25
20020000+01	30000000-01	23950000+04	15000000+02	39
19863000+01	18200000-01	23736000+04	15850000+02	37
13300000+01	19000000-01	12166000+04	15880000+02	18
NO+ 5 1	0 30007000+02	98240300+13	10000000+01	
10000000+01	00000000+00	60000000+01	39982000+05	30000000+01

# APPENDIX B – Continued

58523000+05	60000000+n1	72384000+05	20000000+01	73083800+05
20020000+01	20200000-n1	23771000+04	16350000+02	36
16800000+01	19000000-n1	17400000+04	14500000+02	29
13300000+01	16000000-n1	12200000+04	95000000+01	31
12600000+01	17000000-n1	11400000+04	76000000+01	37
15870000+01	24000000-n1	16089000+04	23300000+02	17
C 30 0	0 12011000+02	71123800+13	00000000+00	
90000000+01	00000000+n0	50000000+01	10194000+05	10000000+01
21648000+05	50000000+01	33735000+05	90000000+01	60360000+05
30000000+01	61982000+n5	15000000+02	64090000+05	30000000+01
68858000+05	15000000+n2	69700000+05	30000000+01	70744000+05
90000000+01	71365000+n5	50000000+01	72611000+05	10000000+01
73976000+05	90000000+n1	75256000+05	50000000+01	77681000+05
90000000+01	78130000+n5	21000000+02	78230000+05	18000000+02
78320000+05	10000000+n2	78600000+05	90000000+01	79318000+05
18000000+02	80400000+n5	12000000+02	81200000+05	50000000+01
81770000+05	10000000+01	82252000+05	53000000+02	83800000+05
10300000+03	84000000+05	30000000+02	84940000+05	60000000+01
85400000+05	50300000+03	86400000+05	19000000+02	86500000+05
C+ 30 0	0 12010000+02	17971820+14	00000000+00	
60000000+01	00000000+n0	12000000+02	43030000+05	10000000+02
74931000+05	20000000+n1	96494000+05	60000000+01	10180000+06
60000000+01	11065000+n6	20000000+01	11490000+06	20000000+01
11653800+06	14000000+n2	11940000+06	60000000+01	13173100+06
12000000+02	13580000+n6	20000000+02	13600000+06	40000000+01
14202400+06	10000000+n2	14555100+06	10000000+02	15046500+06
20000000+01	15723400+n6	60000000+01	16252200+06	12000000+02
16700000+06	10000000+02	16812400+06	20000000+02	16890000+06
20000000+01	17334800+n6	60000000+01	17529300+06	16000000+02
17835000+06	32000000+02	17900000+06	26000000+02	18200000+06
40000000+01	18468900+n6	12000000+02	18645000+06	10000000+02
18860000+06	30000000+n2	19550000+06	20000000+02	19657200+06
C++ 30 0	0 12010000+02	41492250+14	00000000+00	
10000000+01	00000000+n0	90000000+01	52360000+05	30000000+01
10235100+06	90000000+01	13742000+06	50000000+01	14587500+06
10000000+01	18252000+06	30000000+01	23816100+06	10000000+01
24717000+06	30000000+n1	25893100+06	90000000+01	25966200+06
15000000+02	26996000+n6	50000000+01	27684300+06	15000000+02
30910000+06	10000000+01	31172100+06	12000000+02	31870000+06
61000000+02	32255000+n6	50000000+01	32421200+06	12000000+02
32800000+06	31000000+n2	33300000+06	15000000+02	33762600+06
13000000+02	34000000+06	70000000+01	34136800+06	30000000+01
34325600+06	30000000+n2	34500000+06	60000000+02	34660000+06
70000000+01	34800000+06	12000000+02	37660000+06	18000000+02

# APPENDIX B - Continued

38150000+06	13000000+02	38434500+06	34000000+02	38600000+06
C- 1 0	0 12012000+02	58994400+13	00000000+00	
60000000+01	00000000+00			
CO 7 1	0 28011000+02	-11381300+13	10000000+01	
10000000+01	00000000+00	60000000+01	48473900+05	30000000+01
55380000+05	60000000+01	61784600+05	20000000+01	64746500+05
30000000+01	83831000+05	10000000+01	86917800+05	
19313000+01	17480000-01	21702100+04	13461000+02	41
16810000+01	19300000-01	17392500+04	14470000+02	29
13310000+01	16000000-01	12180000+04	95000000+01	31
12615000+01	17000000-01	11377900+04	76240000+01	37
16116000+01	22290000-01	15156100+04	17250500+02	21
20750000+01	33000000-01	21980000+04	13476000+02	40
19610000+01	27000000-01	20820700+04	12092000+02	42
CO+ 3 1	0 28011000+02	12383670+14	10000000+01	
20000000+01	00000000+00	40000000+01	20407500+05	20000000+01
45633500+05				
19772000+01	18960000-01	22142400+04	15164000+02	30
15894000+01	19420000-01	15620600+04	13530000+02	28
17999000+01	30250000-01	17341800+04	27927000+02	15
CN 3 1	0 26019000+02	45605600+13	10000000+01	
20000000+01	00000000+00	40000000+01	91145900+04	20000000+01
25797850+05				
18996000+01	17350000-01	20687050+04	13144000+02	29
17165000+01	17460000-01	18144300+04	12883000+02	34
19701000+01	22150000-01	21641300+04	20250000+02	26
CO2 1 2	0 44011000+02	-39314600+13	20000000+01	
10000000+01	00000000+00			
39060000+00	22000000-02			
66733000+03	00000000+00	66733000+03	00000000+00	13428600+04
00000000+00	23493000+04	00000000+00		

Cases may arise in which the user of this program may be interested in a gas or gas mixture involving fewer than 26 species. If so, only the species cards for the species being considered need be included. The number of species (NUMSP) and number of components (JINDX) are basic inputs and must be adjusted accordingly. The inputs IAR, IN2, IØ2, and ICØ2, which designate the position of Ar, N<sub>2</sub>, O<sub>2</sub>, and CO<sub>2</sub>, respectively, in the species array, must also be adjusted to provide meaningful initial estimates for the species concentrations as required by ROGO. Finally, the number of atoms of a particular component per particle of a species A(I,J) must be designated. For electrons, a charge constraint is used instead of a mass constraint.

The modifications required when the number of species is varied is best illustrated by example. First, consider a CO<sub>2</sub>-N<sub>2</sub>-O<sub>2</sub>-Ar mixture in which double ionization is included (that is, all 26 species are included). A suggested aid to this case is first to construct a table of A(I,J) as follows:

# APPENDIX B – Continued

		1	2	3	4	5
	Component (J) Species (I)	e <sup>-</sup>	Ar	N	O	C
1	e <sup>-</sup>	1	0	0	0	0
2	Ar	0	1	0	0	0
3	Ar <sup>+</sup>	-1	1	0	0	0
4	Ar <sup>++</sup>	-2	1	0	0	0
5	N	0	0	1	0	0
6	N <sup>+</sup>	-1	0	1	0	0
7	N <sup>++</sup>	-2	0	1	0	0
8	N <sub>2</sub>	0	0	2	0	0
9	N <sub>2</sub> <sup>+</sup>	-1	0	2	0	0
10	O	0	0	0	1	0
11	O <sup>+</sup>	-1	0	0	1	0
12	O <sup>++</sup>	-2	0	0	1	0
13	O <sup>-</sup>	1	0	0	1	0
14	O <sub>2</sub>	0	0	0	2	0
15	O <sub>2</sub> <sup>+</sup>	-1	0	0	2	0
16	O <sub>2</sub> <sup>-</sup>	1	0	0	2	0
17	NO	0	0	1	1	0
18	NO <sup>+</sup>	-1	0	1	1	0
19	C	0	0	0	0	1
20	C <sup>+</sup>	-1	0	0	0	1
21	C <sup>++</sup>	-2	0	0	0	1
22	C <sup>-</sup>	1	0	0	0	1
23	CO	0	0	0	1	1
24	CO <sup>+</sup>	-1	0	0	1	1
25	CN	0	0	1	0	1
26	CO <sub>2</sub>	0	0	0	2	1

## APPENDIX B – Continued

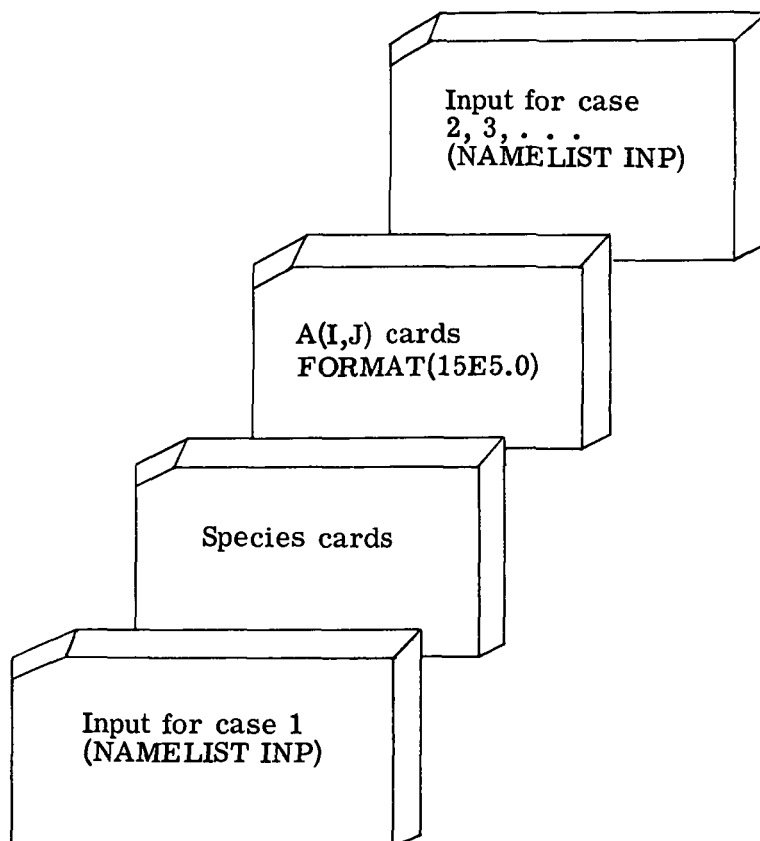
The sequence 0, 1, 0, 0, 0 for species Ar denotes that the only component contained in this species is Ar. (A zero denotes that a particular component does not appear in the species being considered.) In the sequence -1, 1, 0, 0, 0 for Ar<sup>+</sup>, the -1 denotes that Ar<sup>+</sup> is a positive ion, and so forth.

Now, for the mixture being considered, NUMSP = 26, JINDX = 5, IAR = 2, IN2 = 8, IØ2 = 14, and ICØ2 = 26. Naturally, all 26 species decks are included and are placed in the order that they appear in the preceding table of A(I,J). It now remains to read in the A(I,J) as illustrated by the following listing:

1	0	0	0	0	0	1	0	0	0	-1	1	0	0	0
-2	1	0	0	0	0	0	1	0	0	-1	0	1	0	0
-2	0	1	0	0	0	0	2	0	0	-1	0	2	0	0
0	0	0	1	0	-1	0	0	1	0	-2	0	0	1	0
1	0	0	1	0	0	0	0	2	0	-1	0	0	2	0
1	0	0	2	0	0	0	1	1	0	-1	0	1	1	0
0	0	0	0	1	-1	0	0	0	1	-2	0	0	0	1
1	0	0	0	1	0	0	0	1	1	-1	0	0	1	1
0	0	1	0	1	0	0	0	2	1					

Thus, the first card contains the A(I,J) for e<sup>-</sup>, Ar, and Ar<sup>+</sup>; the second, for Ar<sup>++</sup>, N, and N<sup>+</sup>; and so forth.

The sequence of cards following the main program and subroutines is as follows:



## APPENDIX B – Concluded

If the simplified air model used in the previously discussed computer time study is now considered, the table of  $A(I,J)$  takes the following form:

		1	2	3	4
	Component (J) Species (I)	$e^-$	Ar	N	O
1	$e^-$	1	0	0	0
2	Ar	0	1	0	0
3	N	0	0	1	0
4	$N^+$	-1	0	1	0
5	$N_2$	0	0	2	0
6	O	0	0	0	1
7	$O^+$	-1	0	0	1
8	$O_2$	0	0	0	2
9	NO	0	0	1	1
10	$NO^+$	-1	0	1	1

Then,  $NUMSP = 10$ ,  $JINDEX = 4$ ,  $IAR = 2$ ,  $IN2 = 5$ , and  $IØ2 = 8$ . Only the decks for the 10 species considered are included, and these are placed in the order that they appear in the preceding table of  $A(I,J)$ . The  $A(I,J)$  are read in as illustrated by the following listing:

1	0	0	0	0	1	0	0	0	0	1	0	-1	0	1
0	0	0	2	0	0	0	0	1	-1	0	0	1	0	0
0	2	0	0	1	1	-1	0	1	1					

Since the format for reading in the  $A(I,J)$  is the same as for the 26-species case, the first card contains all the  $A(I,J)$  for  $e^-$ , Ar, N, and the first three  $A(I,J)$  for  $N^+$ ; the second card contains the fourth  $A(I,J)$  for  $N^+$ , all the  $A(I,J)$  for  $N_2$ , O, and  $O^+$ , and the first two  $A(I,J)$  for  $O_2$ ; and so forth.

## APPENDIX C

### SAMPLE DATA PRINTOUTS OF COMPUTER PROGRAM

Sample data printouts are given herein. These printouts are for a 26-species air model, a 10-species air model, a 95-percent CO<sub>2</sub>, 5-percent N<sub>2</sub> Venus model, and an 85-percent CO<sub>2</sub>, 1-percent N<sub>2</sub>, 14-percent Ar Mars model, respectively. Procedure ITEST = 3 was used to obtain these printouts.

The headings for the various free-stream and postshock flow conditions of interest correspond to those in the section entitled "SYMBOLS." The units of these flow conditions are also given in this section. The sample computer printouts are as follows:



# APPENDIX C - Continued

01/28/72

GAS MIXTURE DATA REDUCTION PROGRAM OF MILLER  
ALL PHYSICAL QUANTITIES IN MKS UNITS-NASA SP-7012

AIR MODEL(26 SPECIES)

## MEASURED INPUTS

RUN	P1	U1	PT	QT	RHO1	WD	XCJ2	AN2	XO2	XAR
1.000E+00	1.040E+03	6.100E+03	0.	0.	4.850E-03	2.897E+01	3.300E-04	7.808E-01	2.095E-01	9.370E-03

## FREE-STREAM CONDITIONS

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRC
1.040E+03	4.850E-03	7.472E+02	7.602E+05	3.178E+01	1.000E+00	1.359E+00	5.359E+02	6.100E+03	1.130E+01	8.453E+05

## STATIC CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M
1.674E+05	6.229E-02	6.620E+03	1.925E+07	4.399E+01	1.415E+00	1.142E+00	1.752E+03	4.753E+02	2.713E-01

## STAGNATION CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	OTZO	HW	ZN
1.746E+05	6.462E-02	6.644E+03	1.937E+07	4.399E+01	1.417E+00	1.142E+00	1.757E+03	2.742E+07	2.960E+05	1.270E-02

## MOLE FRACTIONS AT STAGNATION CONDITIONS

### SPECIE MOLE FRACTION

E-	4.0696E-04
A	6.6130E-03
A+	1.4978E-07
A++	8.0850E-22
N	2.9828E-01
N+	2.1156E-05
N++	1.7142E-21
N2	3.9864E-01
N2+	6.1787E-06
O	2.8904E-01
O+	2.0531E-05
O++	3.8095E-25
O-	7.3659E-07
O2	1.3728E-04
O2+	2.8967E-07
O2-	4.5576E-10
NO	6.2398E-03
NO+	3.5917E-04
C	3.1329E-05
C+	1.9291E-07
C++	3.6281E-20
C-	5.2360E-11
CO	1.9868E-04
CO+	3.1563E-08
CN	2.6528E-06
CO2	2.3941E-08

01/27/72

GAS MIXTURE DATA REDUCTION PROGRAM OF MILLER  
ALL PHYSICAL QUANTITIES IN MKS UNITS-NASA SP-7012

AIR MODEL(10 SPECIES)

## MEASURED INPUTS

RUN	PI	UI	PT	QT	RH01	WD	XC02	XN2	XO2	XAR
1.000E+00	1.040E+03	6.100E+03	0.	0.	4.850E-03	2.897E+01	0.	7.808E-01	2.095E-01	9.700E-03

## FREE-STREAM CONDITIONS

P	PHC	T	H	S/R	Z	GAME	A	U	M	NRE
1.040E+03	4.850E-03	7.472E+02	7.646E+05	3.178E+01	1.000E+00	1.359E+00	5.399E+02	6.100E+03	1.130E+01	8.452E+05

## STATIC CONDITIONS BEHIND NORMAL SHOCK

P	PHO	T	H	S/R	Z	GAME	A	U	M
1.674E+05	6.229E-02	6.621E+03	1.926E+07	4.398E+01	1.415E+00	1.142E+00	1.752E+03	4.754E+02	2.714E-01

## STAGNATION CONDITIONS BEHIND NORMAL SHOCK

P	RH0	T	H	S/R	Z	GAME	A	QTZO	HW	RN
1.746E+05	6.461E-02	6.645E+03	1.937E+07	4.398E+01	1.417E+00	1.142E+00	1.757E+03	2.742E+07	3.005E+05	1.270E-02

## MOLE FRACTIONS AT STAGNATION CONDITIONS

## SPECIE MOLE FRACTION

FE	4.0425E-04
A	6.8466E-03
N	2.9862E-01
N+	2.1411E-05
V2	3.9850E-01
O	2.8886E-01
O+	2.0736E-05
O2	1.3692E-04
NO	6.2318E-03
NO+	5.0210E-04

# APPENDIX C - Continued

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GAS MIXTURE DATA REDUCTION PROGRAM OF MILLER  
ALL PHYSICAL QUANTITIES IN MKS UNITS-NASA SP-7012

VENUS MODEL

## MEASURED INPUTS

RUN	P1	U1	PT	QT	RHO1	W0	XCJ2	XN2	XO2	XAR
1.000E+00	1.040E+03	6.100E+03	0.	0.	4.850E-03	4.321E+01	9.500E-01	5.000E-02	0.	0.

## FREE-STREAM CONDITIONS

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
1.040E+03	4.850E-03	1.114E+03	7.528E+06	3.761E+01	1.000E+00	1.181E+00	5.333E+02	6.100E+03	1.212E+01	7.336E+05

## STATIC CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M
1.701E+05	7.688E-02	5.845E+03	1.100E+07	6.251E+01	1.968E+00	1.231E+00	1.650E+03	3.848E+02	2.332E-01

## STAGNATION CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	QTZO	HW	3N
1.759E+05	7.900E-02	5.878E+03	1.108E+07	6.251E+01	1.969E+00	1.228E+00	1.653E+03	3.109E+07	8.426E+06	1.270E-02

## MOLE FRACTIONS AT STAGNATION CONDITIONS

### SPECIE MOLE FRACTION

E-	9.0688E-05
A	6.5844E-19
A+	1.3509E-24
N	4.2397E-41
N+	1.7813E-02
N2	1.5280E-07
N2	4.6683E-26
N2	1.4891E-02
N2	2.0328E-08
O	4.8028E-01
O+	5.0564E-06
O+	1.0027E-28
O-	5.2561E-07
O2	1.2943E-03
O2	5.9274E-07
O2-	1.6196E-09
NO	3.0313E-03
NO+	7.0221E-05
C	3.2367E-03
C+	5.1040E-06
C++	1.1922E-20
C-	2.2304E-09
CO	4.7885E-01
CO+	1.0071E-05
CN	9.6076E-05
CO2	3.3266E-04

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GAS MIXTURE DATA REDUCTION PROGRAM OF MILLER  
ALL PHYSICAL QUANTITIES IN MKS UNITS-NASA SP-7012

MARS MODEL

MEASURED INPUTS

RUN	P1	U1	PT	QT	RHO1	WD	XCJ2	XN2	XO2	XAR
1.000E+00	1.040E+03	6.110E+03	0.	0.	4.850E-03	4.328E+01	8.500E-01	1.000E-02	0.	1.400E-01

FREE-STREAM CONDITIONS

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRF
1.040E+03	4.850E-03	1.116E+03	6.674E+06	3.653E+01	1.000E+00	1.198E+00	5.069E+02	6.100E+03	1.203E+01	6.729E+05

STATIC CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M
1.692E+05	7.140E-02	6.474E+03	1.184E+07	6.013E+01	1.906E+00	1.161E+00	1.659E+03	4.144E+02	2.498E-01

STAGNATION CONDITIONS BEHIND NORMAL SHOCK

P	RHO	T	H	S/R	Z	GAME	A	QTZO	HM	RN
1.755E+05	7.365E-02	6.500E+03	1.193E+07	6.014E+01	1.908E+00	1.160E+00	1.662E+03	3.199E+07	7.513E+06	1.273E-02

MOLE FRACTIONS AT STAGNATION CONDITIONS

SPECIE MOLE FRACTION

E-	2.616E-04
A	7.3373E-02
A+	1.3229E-06
A++	3.4724E-21
N	8.9053E-03
N+	5.2758E-07
N++	1.9083E-23
N2	5.3246E-04
N2+	6.5341E-09
C	4.7054E-01
O+	2.8932E-05
O++	1.9298E-25
O-	8.6768E-07
O2	4.5026E-04
O2+	8.7718E-07
O2--	1.0570E-09
NO	3.9920E-04
NO+	2.3569E-05
C	2.5815E-02
C+	1.5080E-04
C++	1.5628E-17
C-	3.1004E-08
CO	4.1927E-01
CO+	5.6546E-05
CN	8.8518E-05
CO2	1.0205E-04

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